


Digitalisation In Action

Developing AI/ML Driven Decision Support in Pulp & Paper

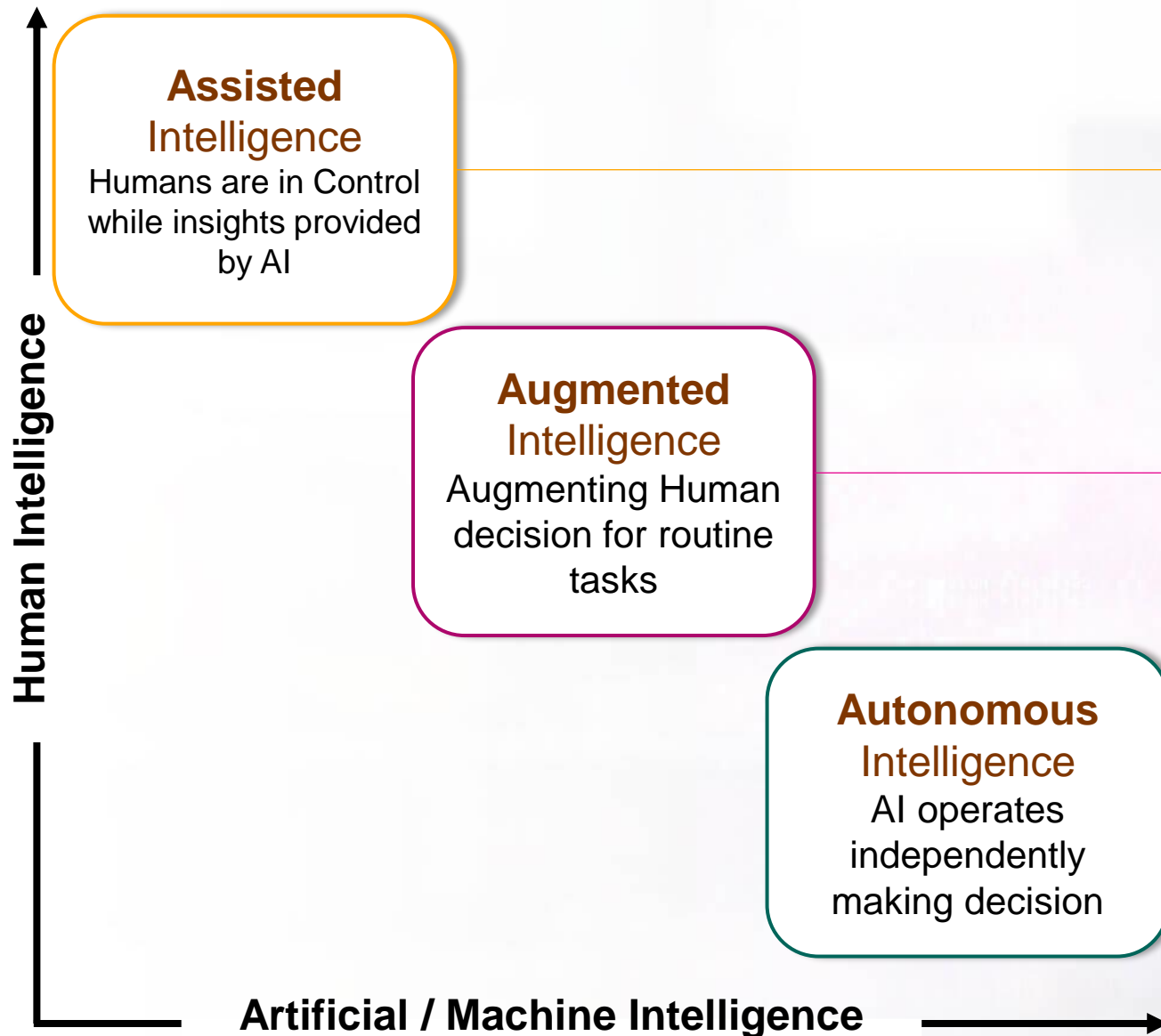
Shankar Das G | BTG India

28th February 2025

MACSsuite
dataPARC

A Voith company



Stages in AI v/s Human Collaboration



Assisted Intelligence | AI as a Tool

- Spelling Correction
- Document Summary
- Mill wide data Integration for real time ETL (Extract, Transform & Load)



Augmented Intelligence | AI as a Partner

- Weather forecasting Tools
- Scenario Analysis (PCA/ PLS)
- Anomaly Detection & Deviation Detection

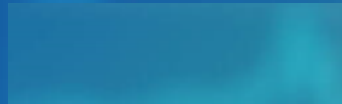


Autonomous Intelligence | AI in the Driver seat

- Self driving cars
- Model predictive Controls Systems

Assisted Intelligence

*Mill-Wide Data Integration for real time ETL
Process (Extract, Transform and Load)*



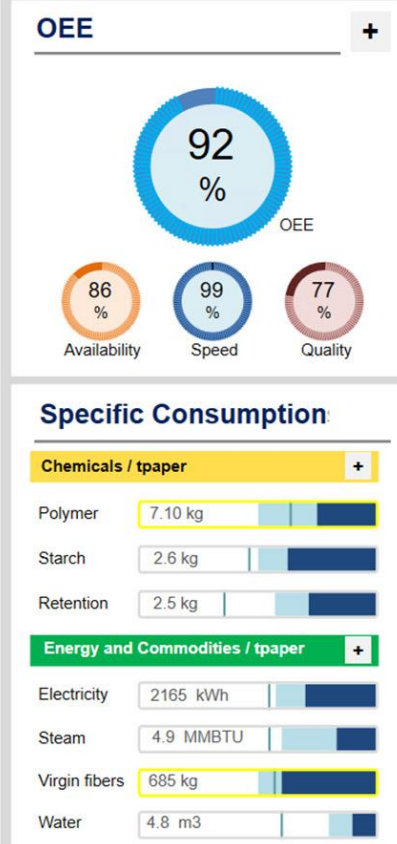
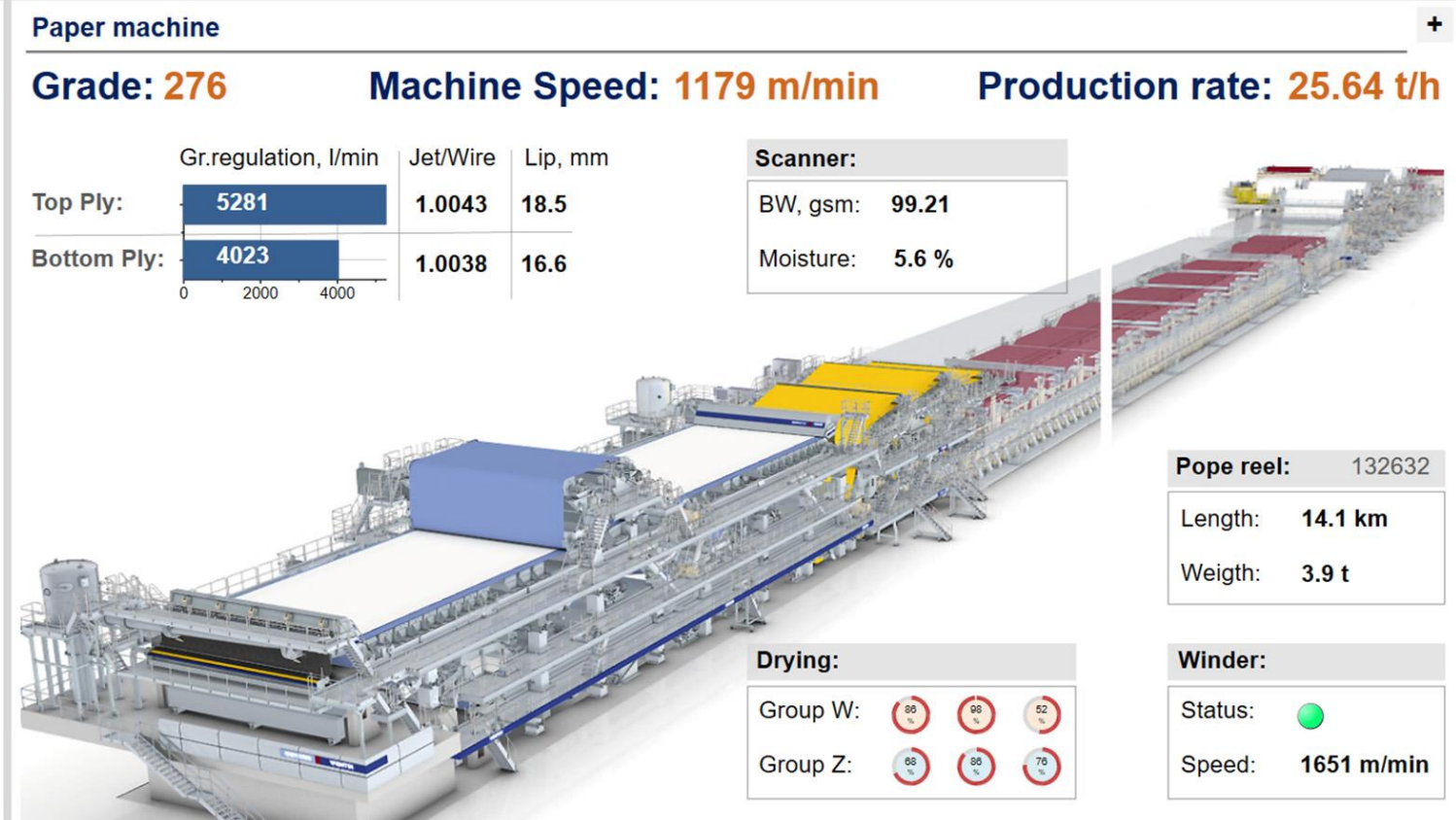
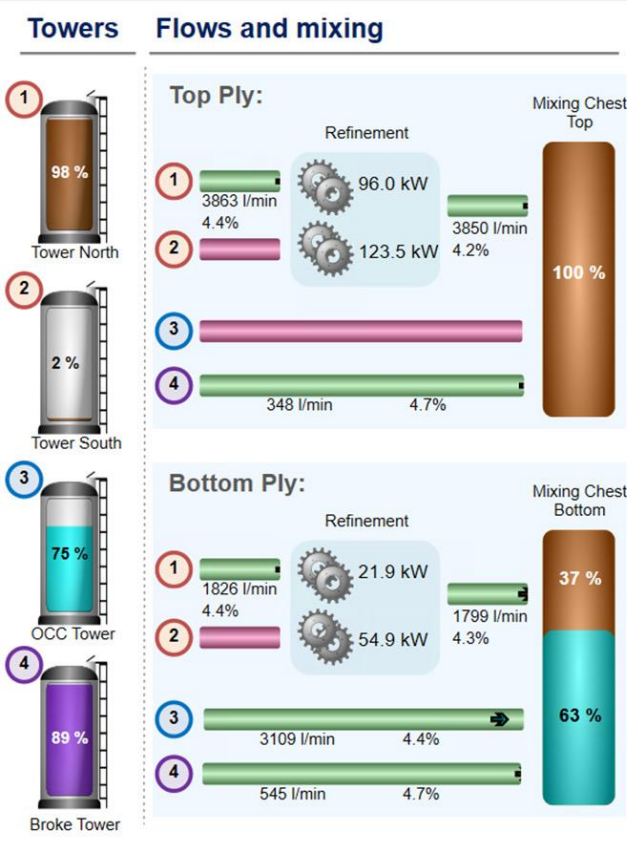
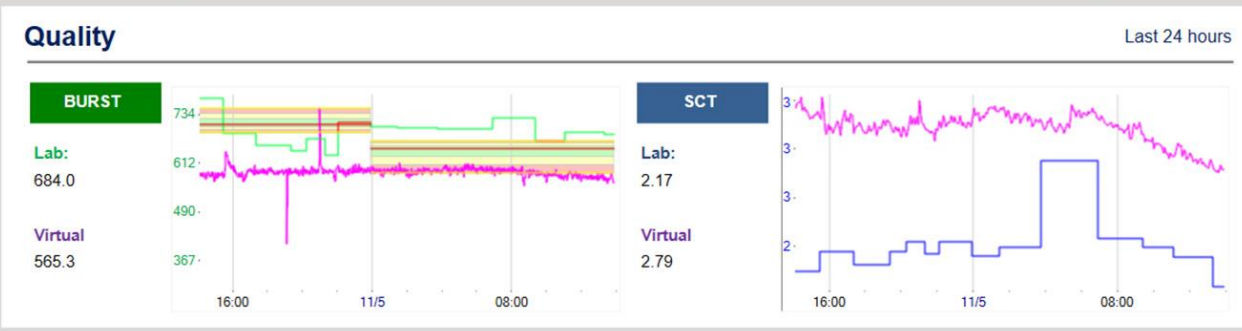
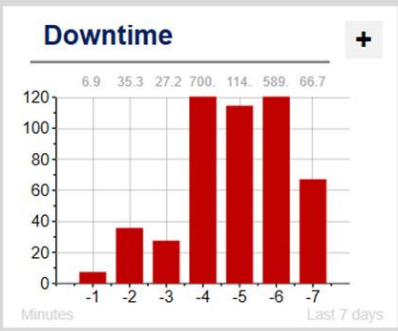
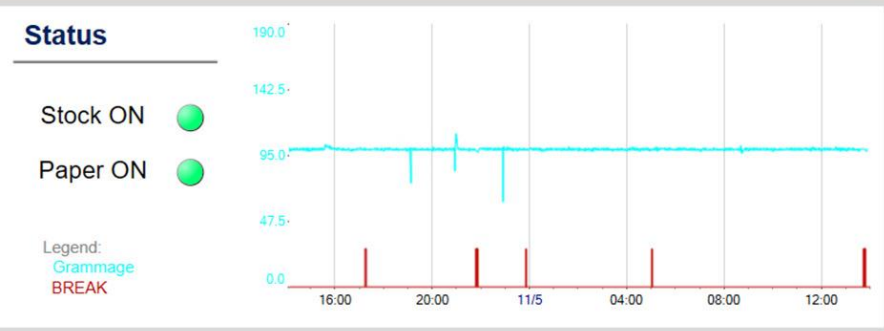
PM Overview Dashboard

Mill-Wide Data Integration

- Need to have all your data in one place
- Breaking down data silos
- Data from all process areas
- Real-time process monitoring
- “Single Source of Truth”



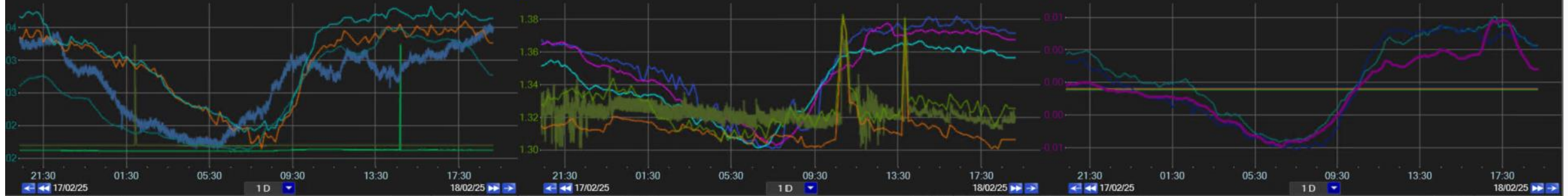
PM Overview Dashboard



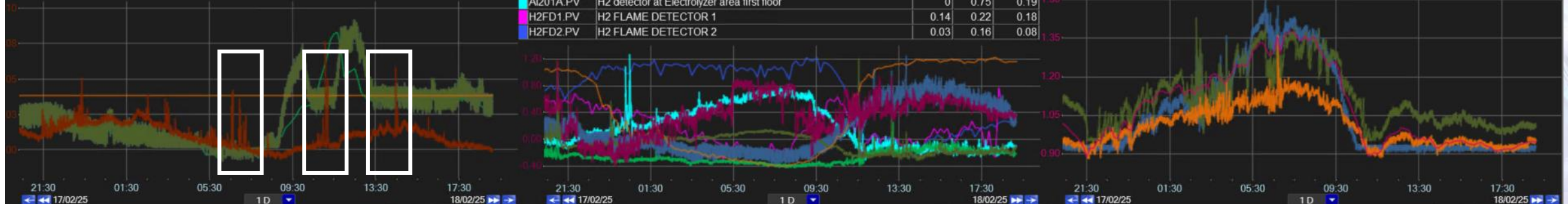
Links

PM @ a Glance	Overview	Profile	Downtime	Asset Monitoring	Pumps
Quality	Centerline	Logbook	Tensile mode	PCA Pumps	PCA TM8

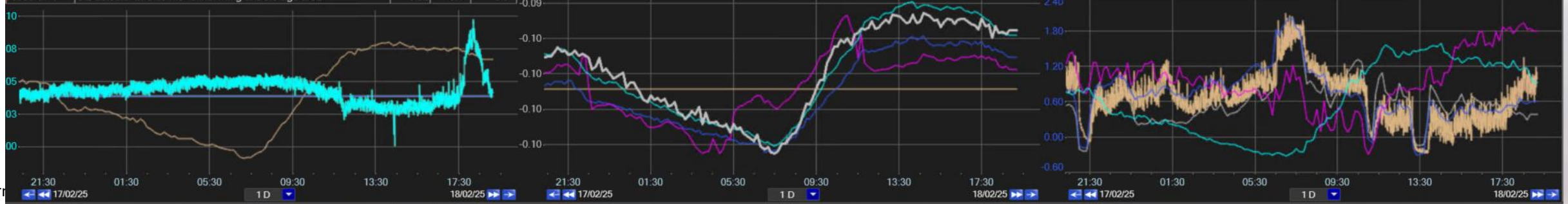
Tag	Description	Min	Max	Current	Tag	Description	Min	Max	Current	Tag	Description	Min	Max	Current
AI230A.PV	CI2 detector at Electrolyzer Room	0.02	0.03	0.03	CL2812.PV	FROM 32% HCL SYNTHESIS UNIT	1.29	1.39	1.33	AI550A.PV	CI2 detector at First floor of Hypo building	-0.63	-0.62	-0.63
AI230B.PV	CI2 detector at Electrolyzer Room	0.01	0.01	0.01	HCI812.PV	FROM 32% HCL SYNTHESIS UNIT	0.01	0.16	0.03	AI550B.PV	CI2 detector at First floor of Hypo building	-3.10	0.15	-1.56
AI540A.PV	CI2 detector at Liquid Chlorine Storage area	-1	6.50	-0.05	CL21731.PV	FROM CL2 GAS ABSORBER BLOWER	0.61	0.79	0.66	AI550E.PV	CI2 detector at 1st floor of Process building	-1.50	1.75	0.03
AI540B.PV	CI2 detector at Liquid Chlorine Storage area	-1.05	-0.73	-0.77	AI550C.PV	CI2 detector at Chlorine compression area	-0.32	-0.31	-0.31	AI550F.PV	CI2 detector at 1st floor of Process building	0.00	0.01	0.01
AI540C.PV	CI2 detector at Liquid Chlorine Storage area	-0.20	1.05	-0.08	AI550D.PV	CI2 detector at Chlorine compression area	0.05	0.07	0.06	AI550G.PV	CI2 detector at 2nd floor of Process building	-0.30	2.95	1.30
AI540D.PV	CI2 detector at Liquid Chlorine Storage area	0.02	0.04	0.03	AI201B.PV	H2 detector at Electrolyzer area first floor	0.23	0.28	0.27	AI550H.PV	CI2 detector at 2nd floor of Process building	-0.01	0.01	0.00



Tag	Description	Min	Max	Current	Tag	Description	Min	Max	Current	Tag	Description	Min	Max	Current
AI821A.PV	CI2 detector at HCl ground floor	-0.02	0.11	0.00	AI601A.PV	H2 detector at H2 Compressor	-0.60	1.40	0.35	AI822A.PV	H2 detector 1st floor at HCL unit	0.80	1.55	0.95
AI821B.PV	CI2 detector at HCl ground floor PRCs	-1.50	1.75	0.02	AI601B.PV	H2 detector at H2 Compressor	-0.42	-0.39	-0.39	AI822B.PV	H2 detector 1st floor at HCL unit	0.70	1.70	0.90
AI821C.PV	CI2 detector at HCl 3rd floor	0.00	0.01	0.00	AI601C.PV	H2 detector at H2 Compressor	-2.30	-0.80	-1.93	AI822C.PV	H2 detector 4th floor at HCL unit	-0.60	0.15	-0.40
AI821D.PV	CI2 detector at HCl 4th floor	0.00	0.01	0.00	AI601D.PV	H2 detector at H2 Compressor	-1.70	-0.70	-1.22	AI822D.PV	H2 detector 4th floor at HCL unit	-0.60	0.15	-0.47
AI821E.PV	CI2 detector at HCl 5th floor	0.03	0.04	0.03	AI601E.PV	H2 detector at H2 Compressor	-0.40	0.85	-0.16					
					AI201A.PV	H2 detector at Electrolyzer area first floor	0	0.75	0.19					
					H2FD1.PV	H2 FLAME DETECTOR 1	0.14	0.22	0.18					
					H2FD2.PV	H2 FLAME DETECTOR 2	0.03	0.16	0.08					



Tag	Description	Min	Max	Current	Tag	Description	Min	Max	Current	Tag	Description	Min	Max	Current
AI550N.PV	CI2 detector at Chlorine Tonner filling and storage area	-0.02	0.11	0.04	AI550M.PV	CI2 detector at Chlorine Tonner filling and storage area	-0.3	-0.3	-0.3	AI601F.PV	H2 detector at H2 Compressor	-0.42	-0.35	-0.38
AI550R.PV	CI2 detector at Chlorine Tonner filling and storage area	-1.50	1.75	0.02	AI550L.PV	CI2 detector at Chlorine Tonner filling and storage area	-0.05	-0.03	-0.03	AI601G.PV	H2 detector at H2 Compressor	4.55	4.57	4.57
AI550Q.PV	CI2 detector at Chlorine Tonner filling and storage area	-0.18	-0.17	-0.17	AI550K.PV	CI2 detector at Chlorine Tonner filling and storage area	-0.34	-0.33	-0.33	AI601H.PV	H2 detector at H2 Compressor	-0.60	2.40	0.59
AI550P.PV	CI2 detector at Chlorine Tonner filling and storage area	-1.30	1.95	0.22	AI550J.PV	CI2 detector at Chlorine Tonner filling and storage area	-1.50	1.75	0.03	AI601I.PV	H2 detector at H2 Compressor	0.10	4.85	2.63
AI550O.PV	CI2 detector at Chlorine Tonner filling and storage area	-1.50	1.75	0.03	AI550I.PV	CI2 detector at Chlorine Tonner filling and storage area	-0.10	-0.09	-0.09	AI601J.PV	H2 detector at H2 Compressor	0.80	3.55	1.71
AI550N.PV	CI2 detector at Chlorine Tonner filling and storage area	-0.02	0.11	0.04										



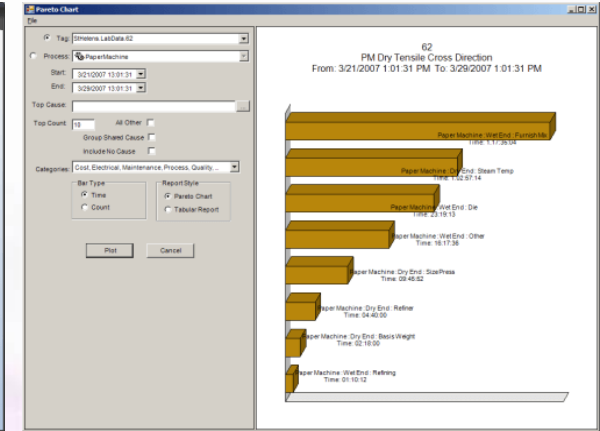
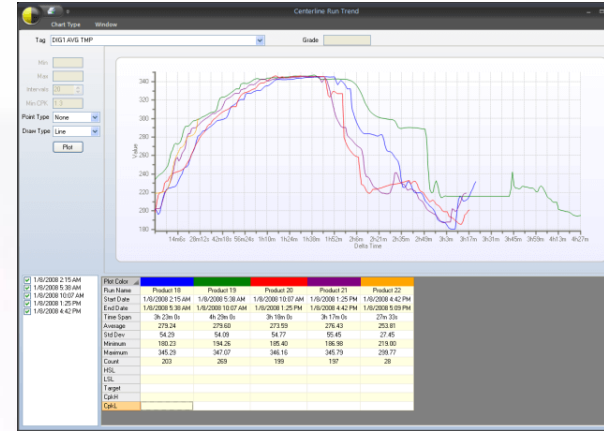
Displays > Main Displays > CRP >

- PARCview
 - Displays
 - 5WhyPreMade
 - Main Displays
 - CPP
 - CRP
 - ELECT
 - Lab
 - Paper Machines
 - Pulp
 - Users
 - My Computer
 - Network
 - Desktop
 - My Documents

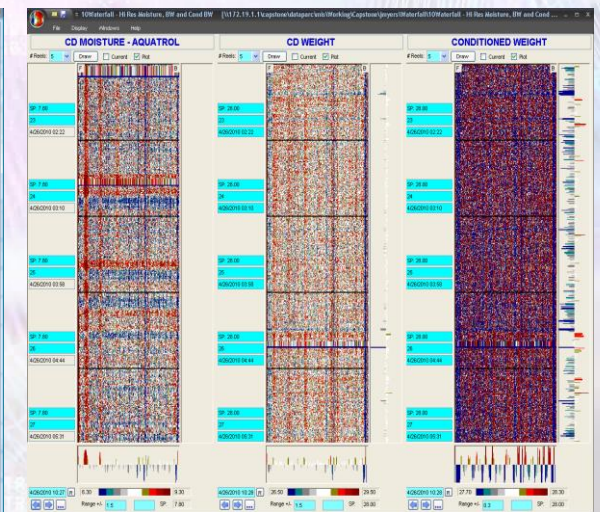
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Black liquor tank level Treands	4/29/2024 5:50:30 AM	PARCview Trend Display
CRP Lab	1/8/2024 12:23:56 PM	Shortcut
CRP MDE	7/19/2024 12:09:15 PM	PARCview Data Entry Display
CRP Process Centerline	6/20/2024 5:24:51 PM	PARCview Centerline Display
CRP_LAB_CenterLine	4/8/2024 9:06:27 AM	Shortcut
Czr Flow & tank Level Treands	5/9/2024 8:29:08 AM	PARCview Trend Display
Daily QC Water Report	1/8/2024 12:23:56 PM	Shortcut
EVAPORATOR CENTERLINE_1	6/4/2024 2:49:57 PM	PARCview Centerline Display
Lime cons	7/1/2024 11:47:20 AM	PARCview Histogram Display
Lime cons	7/2/2024 11:48:12 AM	PARCview Trend Display
New & old RB Steam Parameters	5/5/2024 9:54:29 PM	PARCview Trend Display
New Data Entry	4/23/2024 4:00:24 PM	PARCview Data Entry Display
Totalizers_CRP	7/9/2024 10:16:15 AM	PARCview Centerline Display
White Liquor	11/6/2023 8:37:32 AM	Shortcut

Benefits of AI being an Assisted Intelligence

- Real-time insights empower proactive responses to production challenges.
- Data-driven decisions. Eliminates silos and enables strategic decision-making.
- Reduced downtime through proactive maintenance and root cause analysis.



Description	R	Control	Lower	Target	Upper	12-Dec-2010	11-Dec-2010	10-Dec-2010	09-Dec-2010	08-Dec-2010	07-Dec-2010	06-Dec-2010
Crude Charge Rate												
Crude Charge Rate - MSPD	4.81			4.9		4.83	4.83	4.83	4.9	4.83	4.9	4.9
Crude Sulf Content	88.61			83.16		87.54	88.23	88.23	87.65	87.7	88.88	88.22
Crude Sulf Content - %	85.63			83.16		83.38	83.38	83.46	83.76	84.09	83.42	
Crude Sulf Content - %	86.49			86.21		85.98	85.87	86.43	86.84	87.02	86.8	
Crude Charge Acid F	84.44			84.37		84.36	84.36	84.36	85.36	85.7	87.29	
Crude Charge Sulfur %	23.78			26.37		26.47	26.47	26.6	26.6	26.43	26.36	
Change Crude Group	3.62			3.63		3.58	3.58	3.58	3.57	3.55	3.59	
Distillers												
Crude in Distiller - Temp	336.68			332.34		319.37	292.58	314.77	323.66	322.81	338.6	
Distiller Backpressure - MPD	5.15			5.2		5.21	5.2	5.2	5.21	5.2	5.21	
1st Stage Wash Water Rate - GPM	5.86	5	15	5.12		5.12	5.11	5.11	5.11	5.11	5.11	
1st Stage Wash Water Rate - GPM	41.37			41.06		41.02	41.06	41.72	41.72	42.29	41.05	
1st Stage Wash Water - CAC %	43.21			43.52		43.23	43.26	43.94	43.94	43.64	43.66	
Distiller Wash - VCLTS	128.88			121.83		121	121.81	128.58	128.63	121.37	121.18	
2nd Stage Wash Water Rate - GPM	192.13	5	15	193.33		193.88	193.88	193.88	193.88	193.88	193.88	
2nd Stage Wash Water Rate - GPM	799.31			791.81		696.53	693.77	699.66	1000.17	999.82	218.44	
2nd Stage Wash Water - CAC %	191.98			191.98		191.98	192.01	192.01	192.01	191.99	192.75	
Distiller Wash - pH	192	5	6	192		192	192	192	192	192	192	
Distiller Wash - VCLTS	18.58			11.21		8.44	10.74	12.95	18.88	24.62	5.12	
Inlet Effluent Chem - 1st Stage - GPM	12.89			13.82		13.52	12.87	14.87	22.64	38.18	11.24	
Oil in Water - ppm	3.64			2.96		3.9	3.88	3.89	3.92	2.62	4.03	
Sulfur Sulf Content - Molar	191.96	1		191.99		191.99	192	192.01	192.04	191.96	181.82	
Oil in Washed Crude - %	192			192		192	192	192	192	192	192	
At Header												
Header Inlet Temperature of	8.9			0.92		0.99	0.96	0.97	1.62	1.84	6.97	
Header Outlet Pressure - gpm	18.49			18.69		9.45	9.54	10.24	8.41	7.3	4.47	
Header Outlet Temp - °F	-0.01			-0.01		-0.01	-0.01	-0.01	-0.01	-0.01	-0.01	
Header Charge Flow - (Sum of FC) - MSPD	11.85			11.14		12.27	13.07	11.92	12.23	11.89	11.89	
Header Utilization - SCF/BBL	2.84			2.86		2.67	2.71	2.81	2.88	2.83	2.12	
Header Fuel Gas Pressure - PSIG	141			146.78		146.27	146.27	144.01	146.27	144.42	242.18	
Header Excess O2 - %	63	2.5	3	63.03		68.38	70.7	65.9	66.76	62.51	68.14	
Header Acid Concentration - °C	463.91			461.24		441.66	598.08	562.26	625.96	602.31	729.73	
Header Acid Concentration - °C	1.31			1.45		1.58	1.63	1.54	1.62	1.64	1.36	
Overhead Accumulator												
Overhead Accumulator Pressure - PSIG	256.46			481.22		447.5	454.89	483.49	388.77	388.77	571.95	
Overhead Accumulator Temperature - F	442.19			448.5		448.13	431.02	452.94	424.19	420.34	412.74	
Overhead Condensate pH	482.14			488.43		488.65	478.78	488.57	484.57	482.07	488.41	
Total Chloride - ppm	473.76			476.76		476.29	477.39	480.64	479.68	479.79	479.79	
Calculated Salt Flow - F	2.02			2.05		2.11	2.04	2.08	2.08	2.11	2.08	
Approach to Water Desorption - F	29.2			30.09		31.51	25.34	30.05	30.54	27.3	26.18	
Overhead Wash Water Rate - gpm	1.85			1.85		1.1	1.06	1.05	1.11	1.05	1.1	
Water Wash Temperature Drop - Before After - F	331.48			265.21		273.97	265.49	279.6	264.54	264.99	241.58	
Tower Distillation												
Tower Overhead - °F	157.96			158.62		154.88	157.2	157.1	155.76	156.34	155.42	
Tower Middle Dist - °F	179.27			172.89		174.52	176.26	176.88	175.27	174.44	171.86	
Tower Base - °F	360.07			358.22		359.12	358.27	357.1	357.76	356.68	356.21	
Distill Dist - °F	348			339.01		329.96	296.18	280.6	261.95	276.16	283.13	



Augmented Intelligence

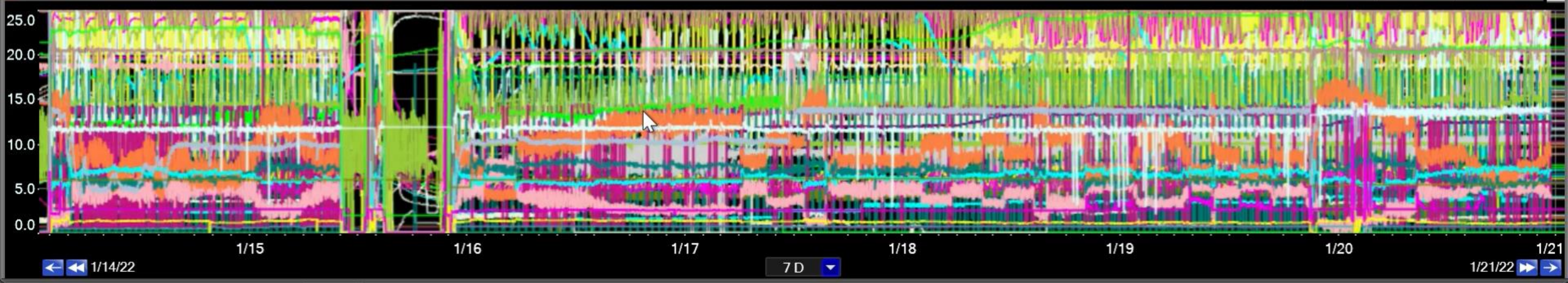
*Anomaly Detection & Deviation Detection using
Principle Component Analysis*



Anomaly detection using PCA models

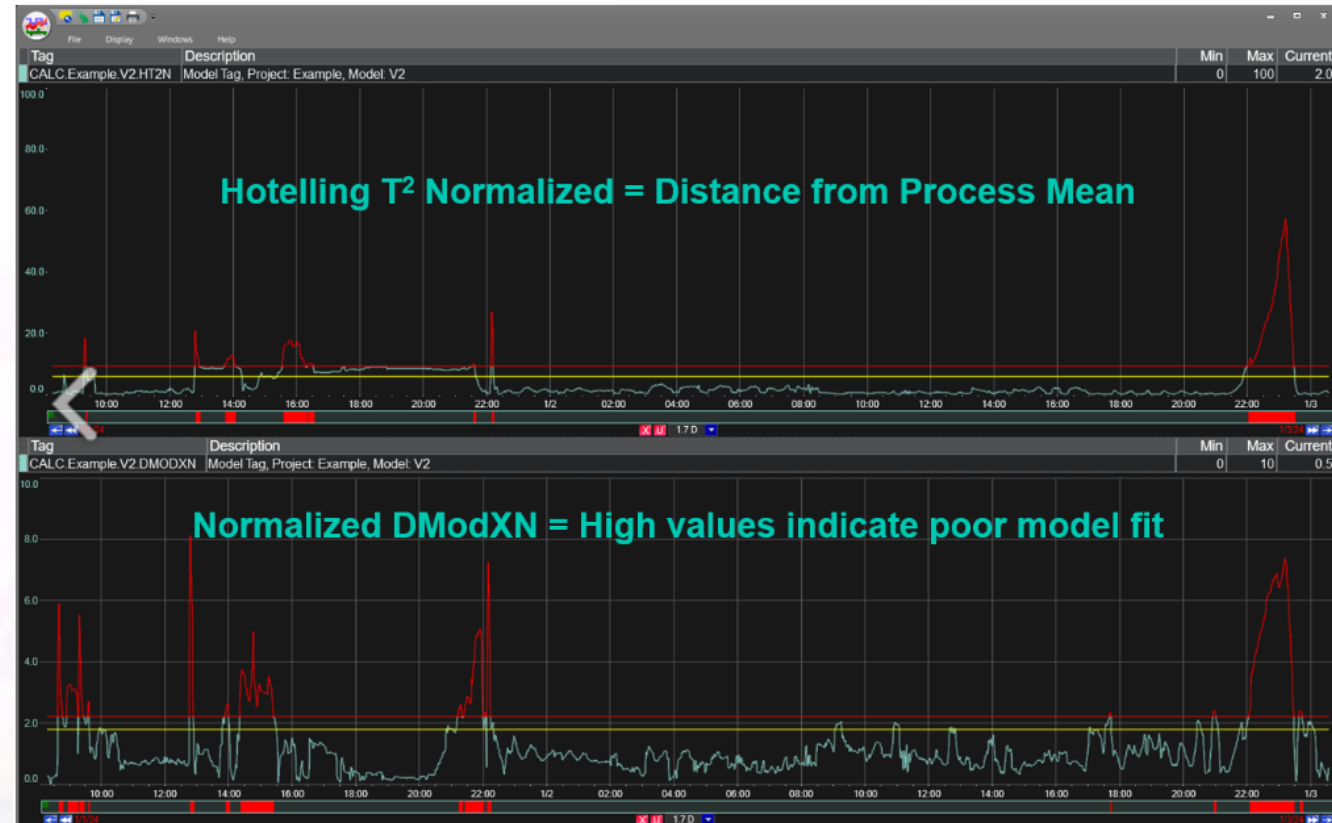
- PCA technique aims to simplify complex datasets by reducing their dimensionality while retaining most of its information.
 - It does this by identifying new, uncorrelated variables called principal components & its variance.
 - Principal components are linear combinations of the original variables and are ordered on its magnitude
- Identify Variables
 - Establish Time Periods for Evaluation
 - Generate the PCA Modelled Data
 - Evaluate the PCA Model
 - Using PCA Model as a continuous data TAG

Tag	Description	Min	Max	Current
pr:8TM-MSC1	TM8 Machine Speed PV	0	6560	5470
pr:FIC-T80100	TM8 Refiner Outlet Dilution Flow PV	0	200	20.7
pr:JIC-T80100	TM8 Refiner Specific Energy Control PV	0	100	4.5
pr:JIC-T80100	TM8 Refiner Load PV	0	100	563.6
pr:SDC-80MRL	TM8 Crepe Ratio PV	0	100	22.2
pr:FCI-T85800	TM8 Yankee Coating Ratio Control PV	0	100	2.9
pr:VIC-T80100	TM8 Refiner Chest Consistency PV	3	5	4.07
pr:TAI-T80101	TM8 Refiner Outlet Temperature PV	0	100	124.0
pr:8TM-BWRL	TM8 Basis Weight PV	0	25	13.9
pr:FIC-T80100	TM8 Refiner Outlet Flow PV	0	1500	424
pr:FIC-T80100	TM8 Refiner Outlet Recirc. Flow PV	0	1000	224
pr:FIC-T80100	TM8 Refiner Outlet Dilution Flow PV	0	200	20.7
pr:FIC-T80201	TM8 Broke Deflaker Outlet Flow PV	0	400	155
pr:FIC-T80201	TM8 Broke Recirculation Flow PV	0	750	116
pr:FIC-T80500	TM8 Broke Pulper Inlet Flow PV	0	800	327
pr:FIC-T80600	TM8 Secondary Screen Reject Flow PV	0	100	7.6
pr:FIC-T80600	TM8 Secondary Screen Accepts PV	50	600	500



Benefits of AI being an Augmented Intelligence

- Root cause analysis with Facts over intuition.
- Provide early warnings for potential quality or maintenance issues.
- Moves from reactive to proactive problem solving



TR/01 #83
TR/01 #83

SEARCH TR/01 #83
SEARCH TR/01 #83

Autonomous Intelligence

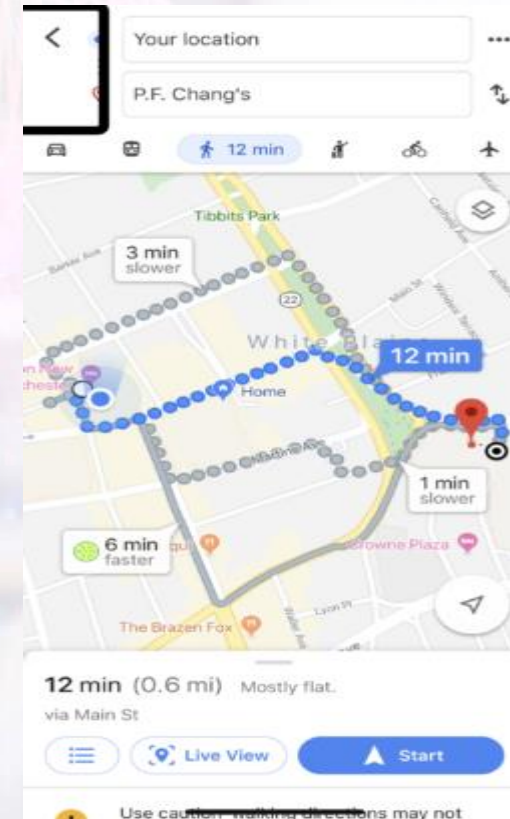
Making decisions and actions without direct human intervention using Model Predictive Advanced Process Controls

Static Model v/s Dynamic Model

A static model represents a system at a specific point in time based on Historical data. **It doesn't account for changes over time.**



A dynamic model represents a system as it evolves over time. **It captures the behavior and interactions within the system.**



Dynamic Model = Mathematical Model

- Mathematical model uses mathematical equations and expressions to represent a process.
- It focuses on the underlying relationships of different variables involved within the Process.
- Used to predict the behavior of Process bases on relation between variables .

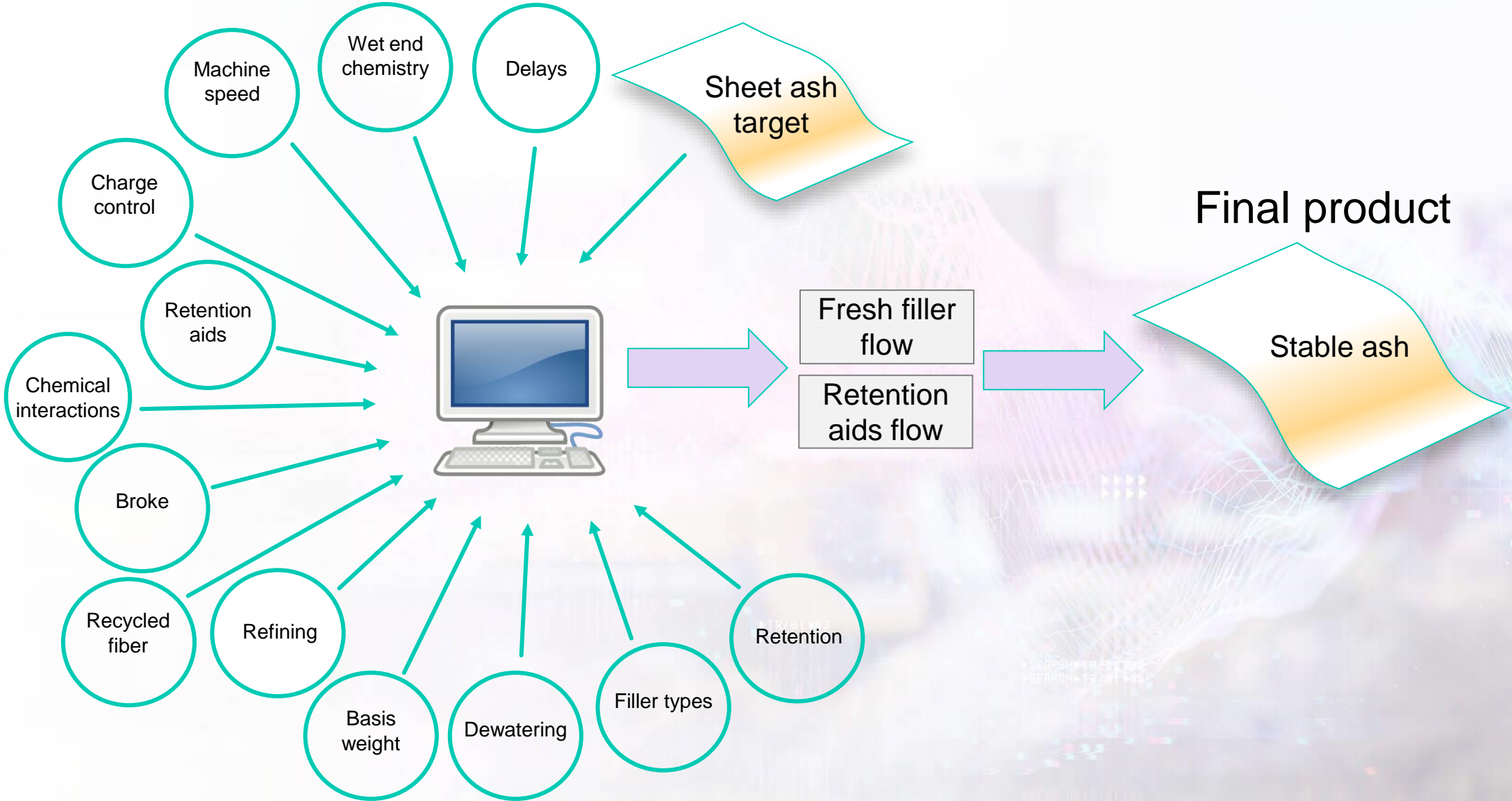


- Historical Data
- Pattern Recognition
- Forecasting



- Realtime measurements
- Modelled Process relationship
- Prediction

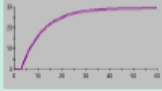
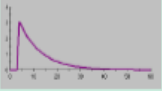
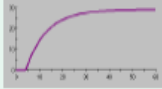
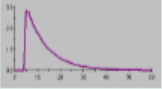
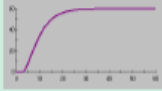
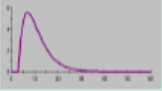


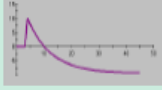
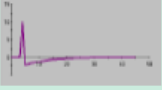
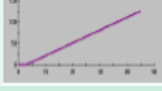
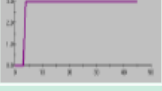
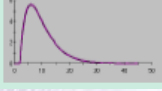
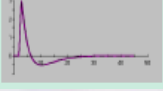
Model Predictive Paper Ash Control



Model Predictive Ash Control Matrix

		Control Variables (CV)		Constraints (CT) (if needed)	
		Tray Water Consistency (RET)	Base Sheet Ash (Scanner)	Post Carb ThickStock Ash (TCR)	Base Sheet Formation* (Scanner)
MV's	Carbonate Flow	+	-	+	-
	Polymer Flow	+	-	+	-
FF's	Broke % Ash	+	-	+	-
	Broke % Furnish	+	-	+	-
	WSA	+	-	+	-
	TiO2 Dosage	+	-	+	-

The matrix presented here illustrates the positive and negative relationships within the system. It is important to note that this matrix is not realistic and has been simplified to maintain confidentiality.

Model Type	Equation	Step	Impulse
1 st Order w/delay	$y(t) = 0.89y(t-1) + 3.06u(t-5)$		
1 st Order w/fractional delay	$y(t) = 0.89y(t-1) + 2.82u(t-5) + 0.27u(t-6)$		
2 nd Order Over Damped	$y(t) = 1.55y(t-1) - 0.6y(t-2) + 3.0u(t-4)$		
2 nd Order Under Damped	$y(t) = 1.3y(t-1) - 0.6y(t-2) + 3.0u(t-4)$		
Non-Minimum Phase	$y(t) = 0.89y(t-1) + 10.1u(t-4) - 11.2u(t-5)$		
Integrator	$y(t) = 1.0y(t-1) + 2.99u(t-4)$		
Transient	$y(t) = 1.55y(t-1) - 0.6y(t-2) + 3.0u(t-3) - 3.0u(t-4)$		

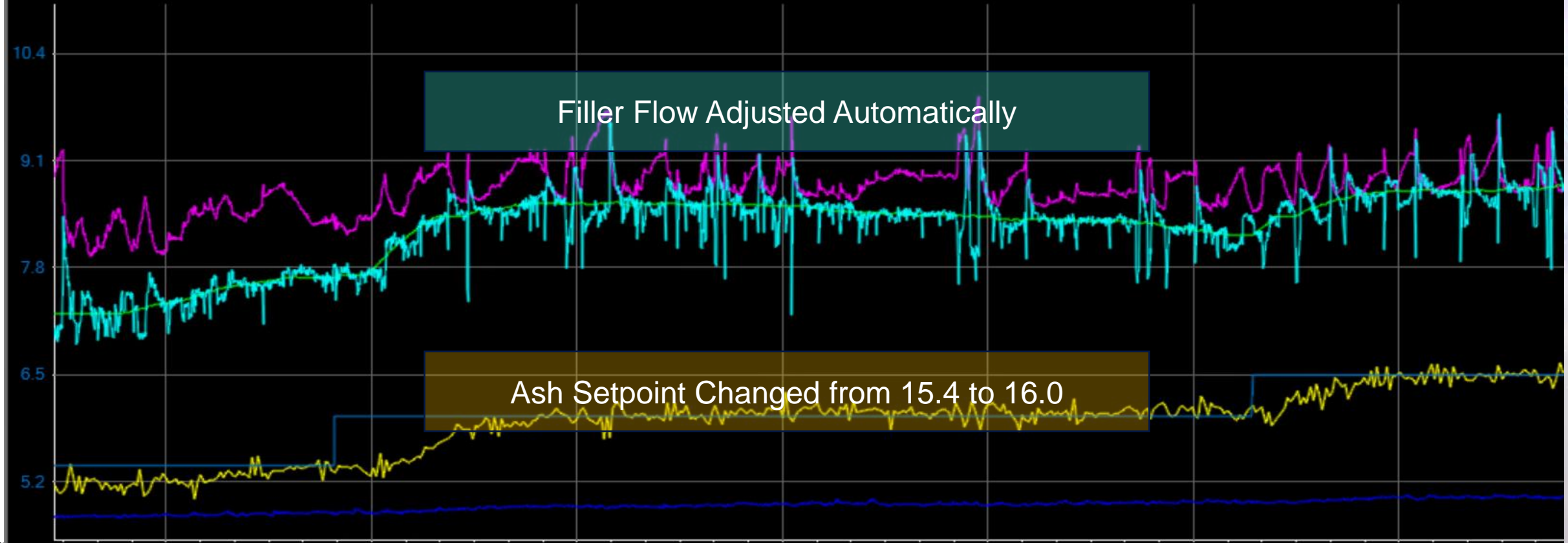
Variable Types:

MV → Manipulated Variable

FF → Feed Forward Variable

MACSash control Results

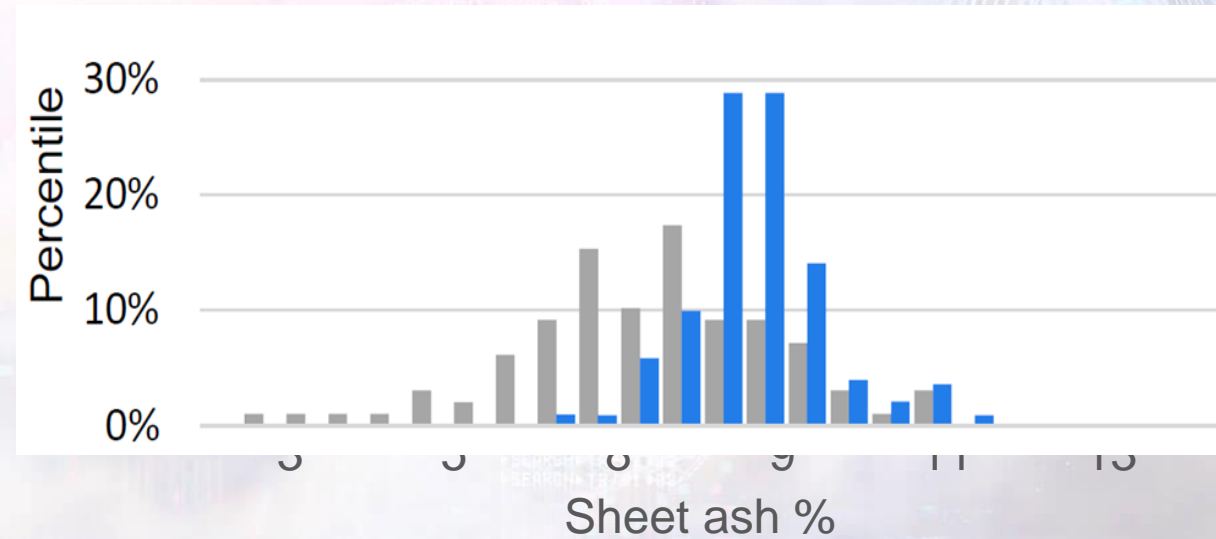
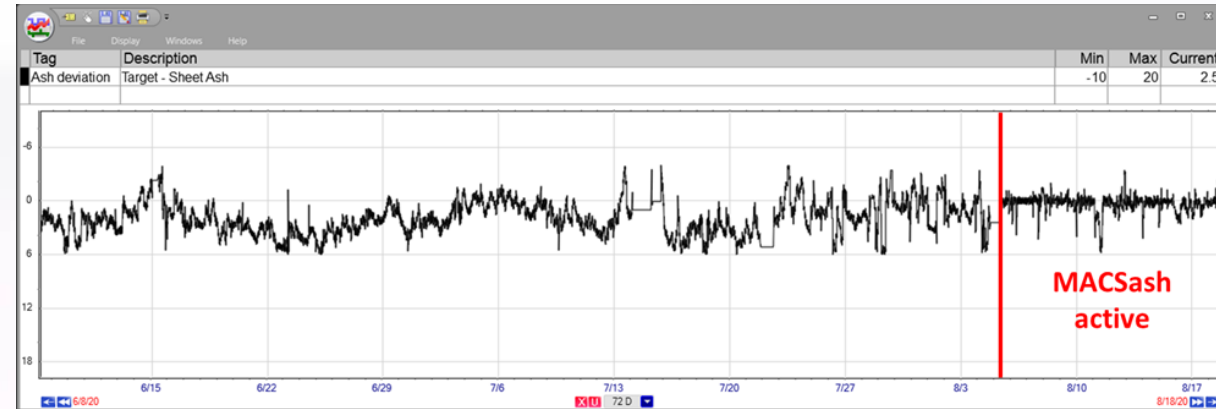
Tag	Description
PM03-CLF1-01	CaCO3 Flow
PM03-CLF1-02	CaCO3 Flow
PM03-CLF1-03	CaCO3 Flow
Niklasdorf.Valn	scanner FP ash MD
CSIC413601.2	Ash White Water - RET
CSIC413603.2	Ash Machine Chest 1 - TCR
MACS_SheetA	MACS Sheet Ash Target



Benefits of AI being an Autonomous Intelligence

(MACSash Case)

- Reduced variability enabled higher ash setpoint, while maintaining wet strength targets.
- *MACSash project led to average savings of 5,5 €/t*
- Ash variation reduction by 80%
- Average sheet ash increased by 1 %



Conclusion

Aspect	Assisted Intelligence	Augmented Intelligence	Autonomous Intelligence
Description	Support Tool	Active Collaborator	In Control
Decisions	By Humans	Human + AI Guidance	AI with Human Oversight
Complexity	Low	Moderate	High
Whole Process Suitability	Yes	Yes	Selected Areas
Software Coding	No	No	Yes
Communication	OPC / SQL	OPC / SQL	OPC
Tools	PARC View	PARC Model	MACS
Intangible Benefits	Single Source of Truth	Faster Analysis	Less Manual Intervention
Quantifiable Benefits	TBA	TBA	\$2-\$8/Ton Savings

Key to Success:

- ✓ Early Adoption
- ✓ Leveraging Existing Tools
- ✓ Human-AI Collaboration



MACSsuite

dataPARC

BTG

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