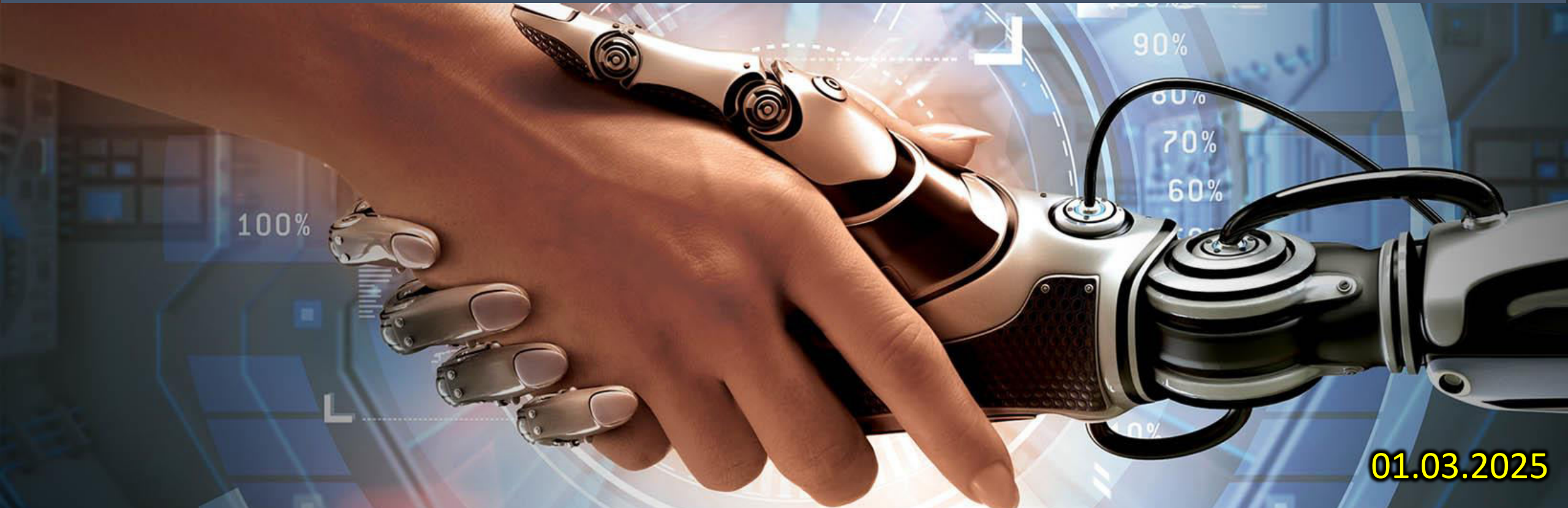




Seshasayee Paper and Boards Limited, Erode

AI-Driven Pulp Bleaching: Achieving Significant Reductions in Chemical Usage



01.03.2025

A Case Study at Seshasayee Paper and Boards Limited (SPB)

Team: Mr. B V Sivakumar & Mr. D.Radhakrishnan



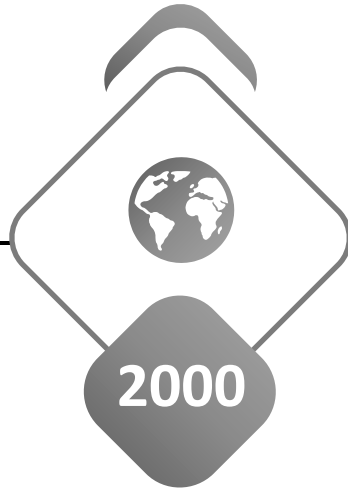
SPB's commitment for Excellence



1996



9001:2015



2000



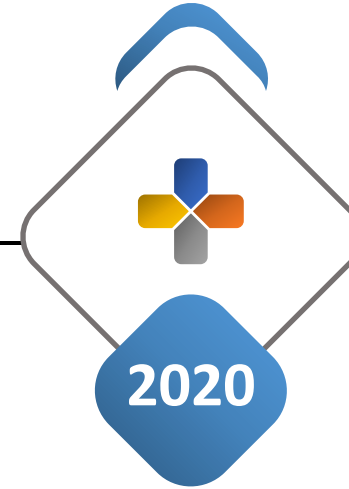
14001:2015



2010



2017



2020



45001:2018



2024



50001:2018

“ Without standards & Measurements, there can be no improvement ”

The Pulp & Paper Industry Challenge



Resource utilisation



Resource Raw material availability



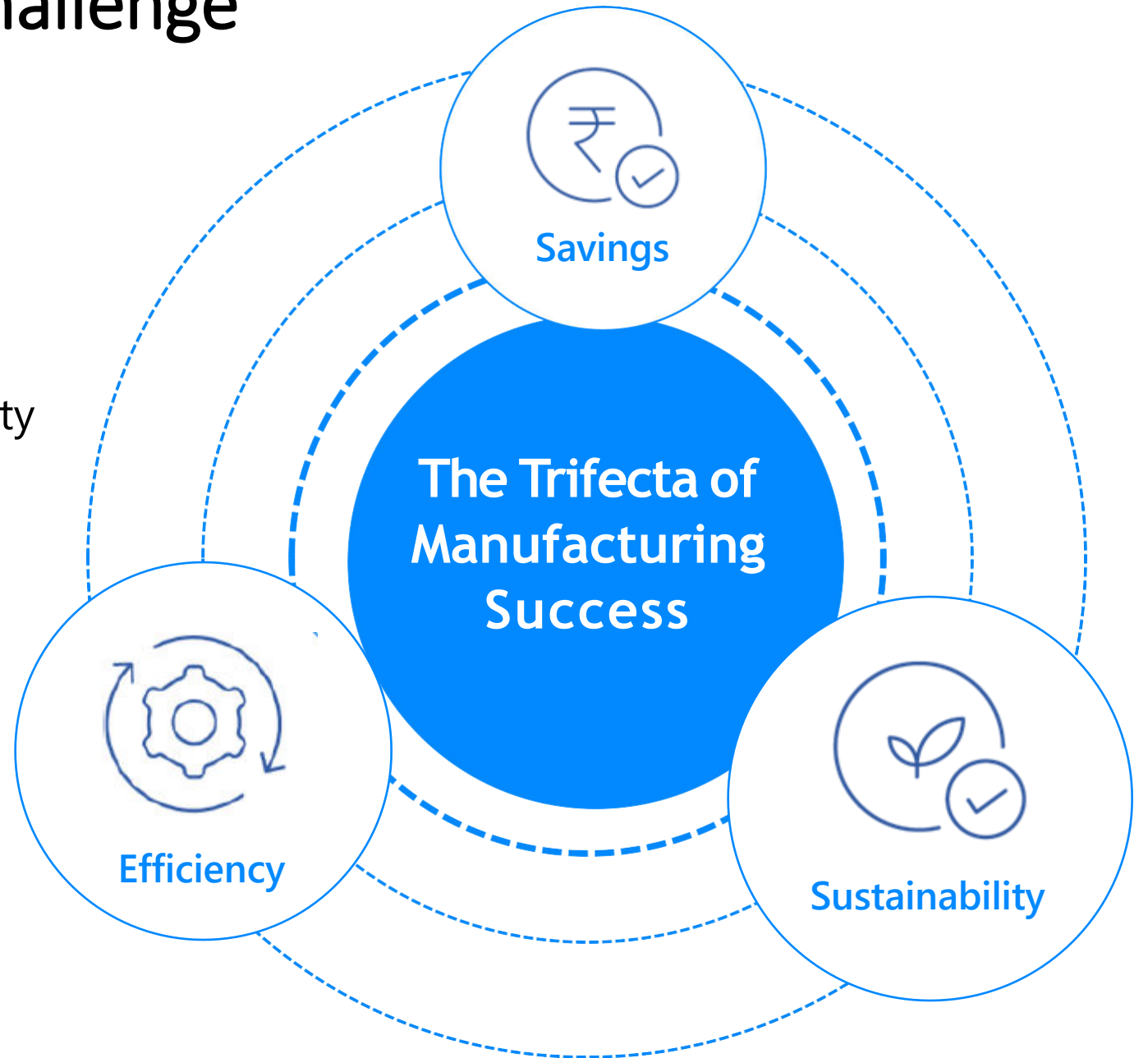
Adaptability and scalability



Quality compliance utilization



Supply chain efficiency



The Bleaching Process & Traditional Control

- Remove lignin and impurities to achieve desired brightness.

Limitations of Traditional Methods

- Reliance on fixed parameters
- Operator experience
- Difficulty adapting to raw material
- Process variability
- Over-consumption of bleaching chemicals
- Inconsistent product quality
- Increased environmental burden



Cooking: RDH Technology
ODL: 2 stage
Bleaching sequence: D0->Eop-> D1
ISO Brightness: 86

The Power of AI



Resource Optimisation

Real-time monitoring and insight-driven decision making to reduce wastage, identify inefficiencies, and enable cost savings



Streamlined Operations

Transparency and accuracy in data to promptly identify incidents, facilitating swift issue resolution.



Unified Central System

A role-based platform for data tracking across all manufacturing stages, ensuring easy access to records for informed process optimization.



Sustainability Reporting

Easily accessible data for streamlined audit and sustainability reporting



Production Efficiency

A streamlined system ensuring uniform quality to elevate customer satisfaction

- AI offers precise control, optimized chemical usage, enhanced product consistency, and improved sustainability.
- Learns from vast amounts of data to identify complex relationships.
- Enables dynamic adjustments to process parameters.

AI-Driven Solution in Bleach Plant operations

The objective of the bleach controller

- Reduce final brightness variability.
- Minimize the chemical consumption maintaining the final brightness

Controlled by

- Optimal pH set points for the inlet of D0, and the inlet of Eop stages.
- Optimal Acid, Chlorine Dioxide, Caustic dosages in each stages of the bleach plant to minimize variability in final pulp brightness.

Software used:

- MACS - Multivariable Advanced Control System software is a Model based Predictive Controller (MPC).

AI Solution Overview

- The key components:
 - Machine learning algorithms.
 - Advanced data analytics.
 - Predictive modeling.

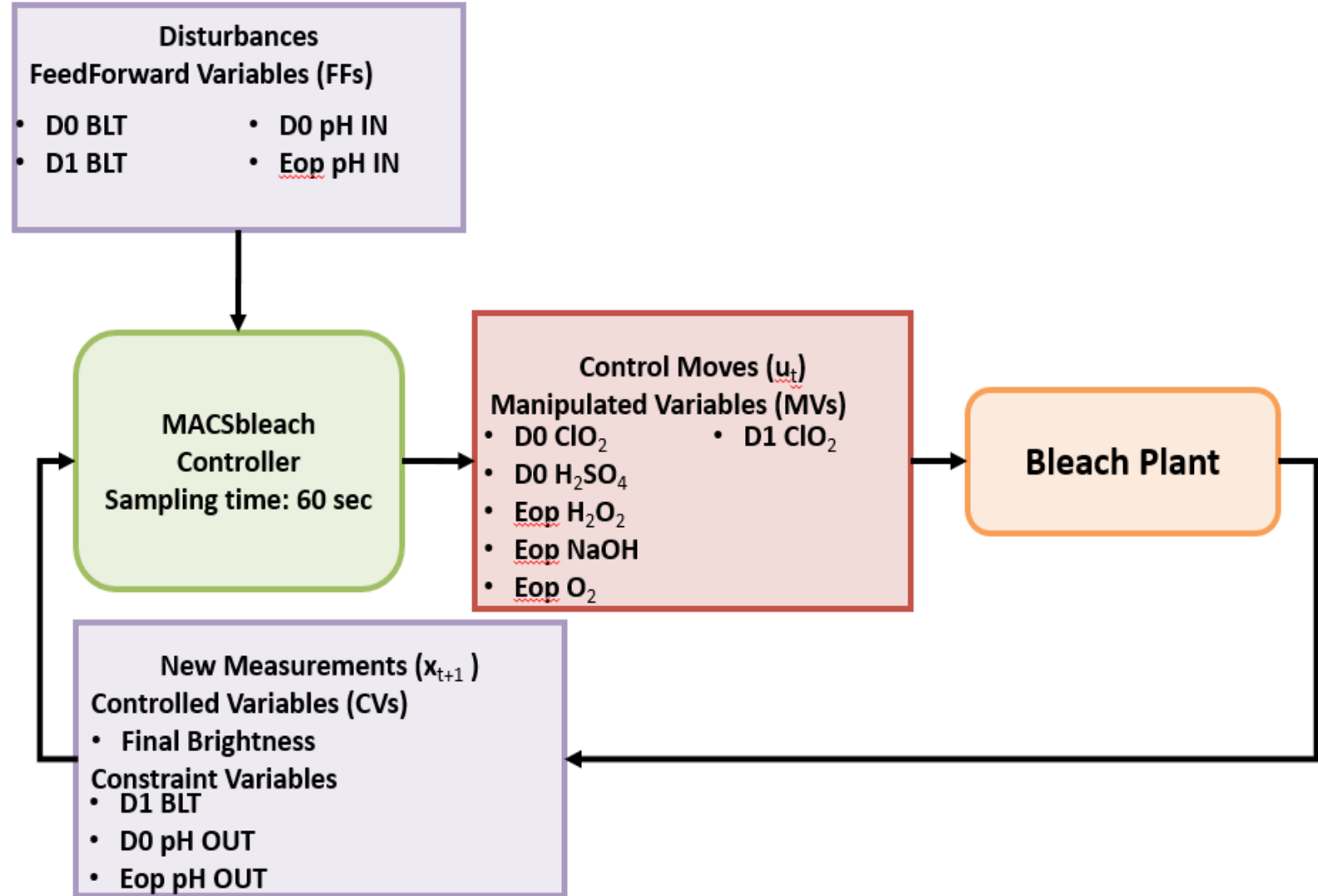
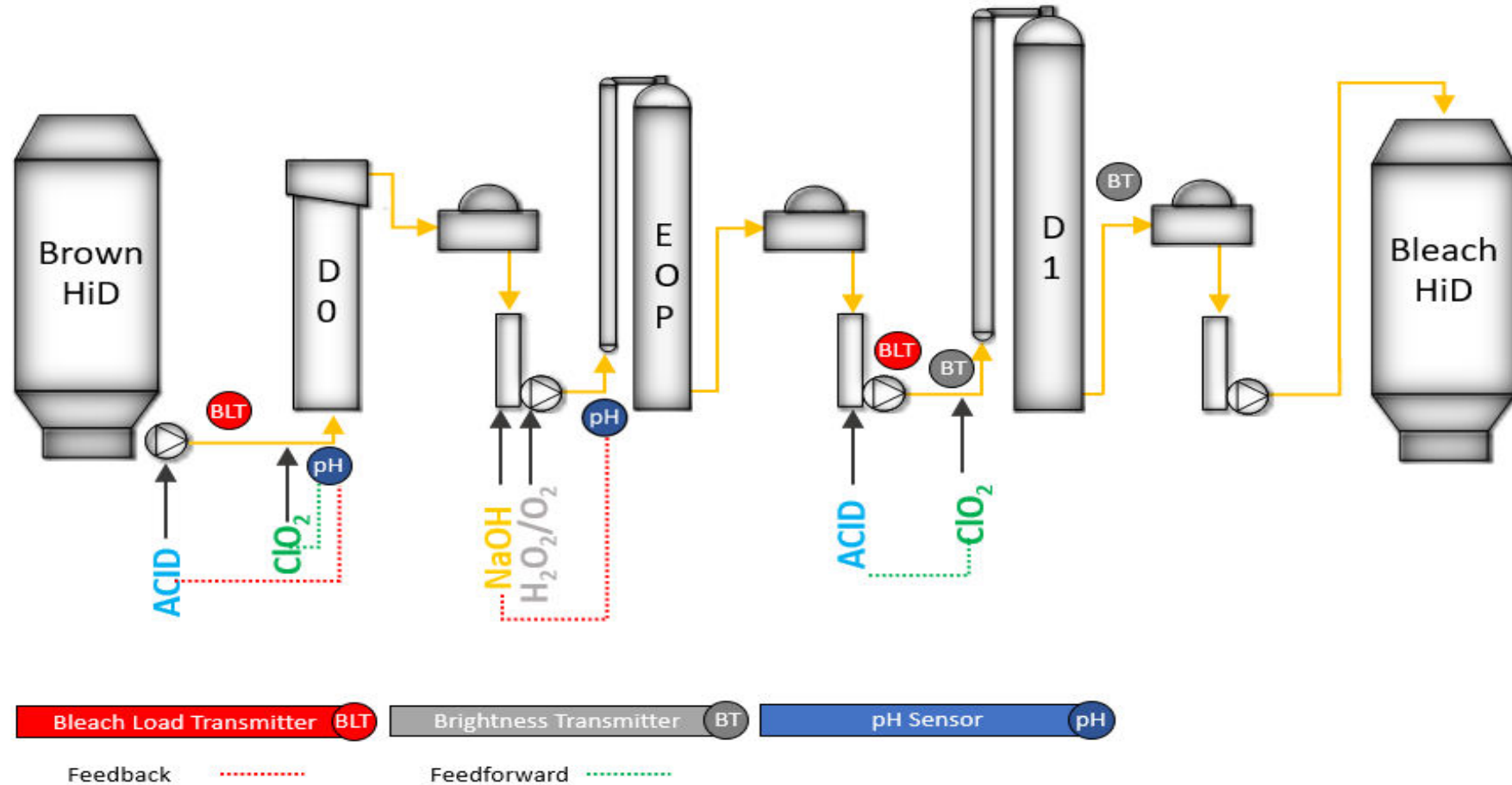


Diagram illustrating
The AI system architecture.

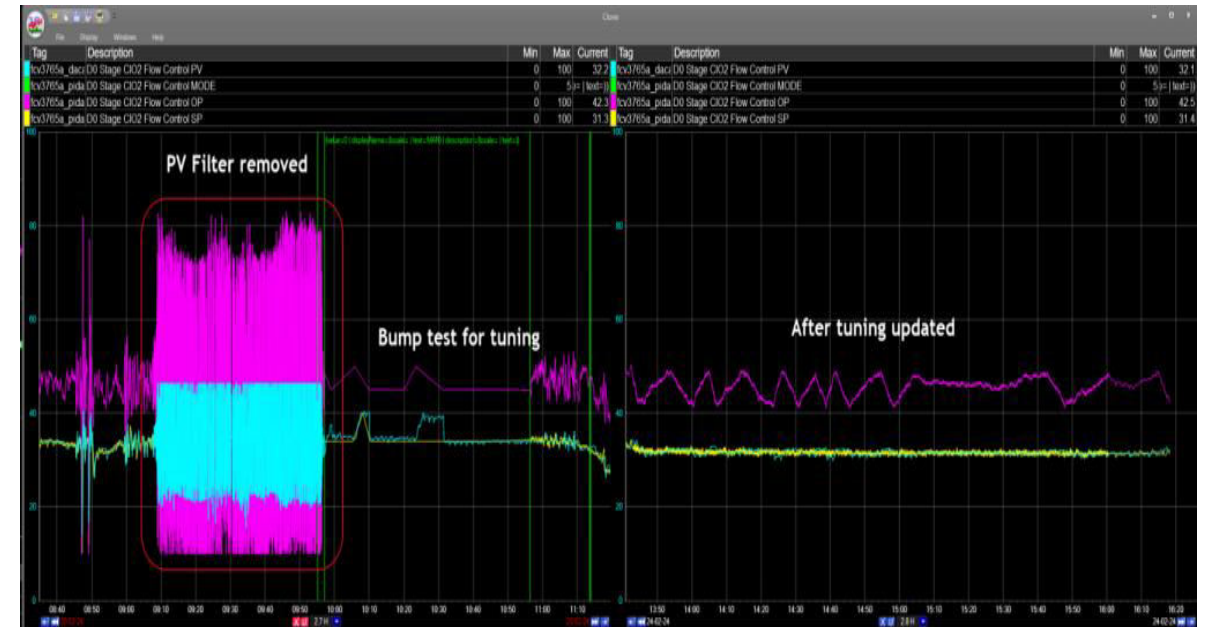
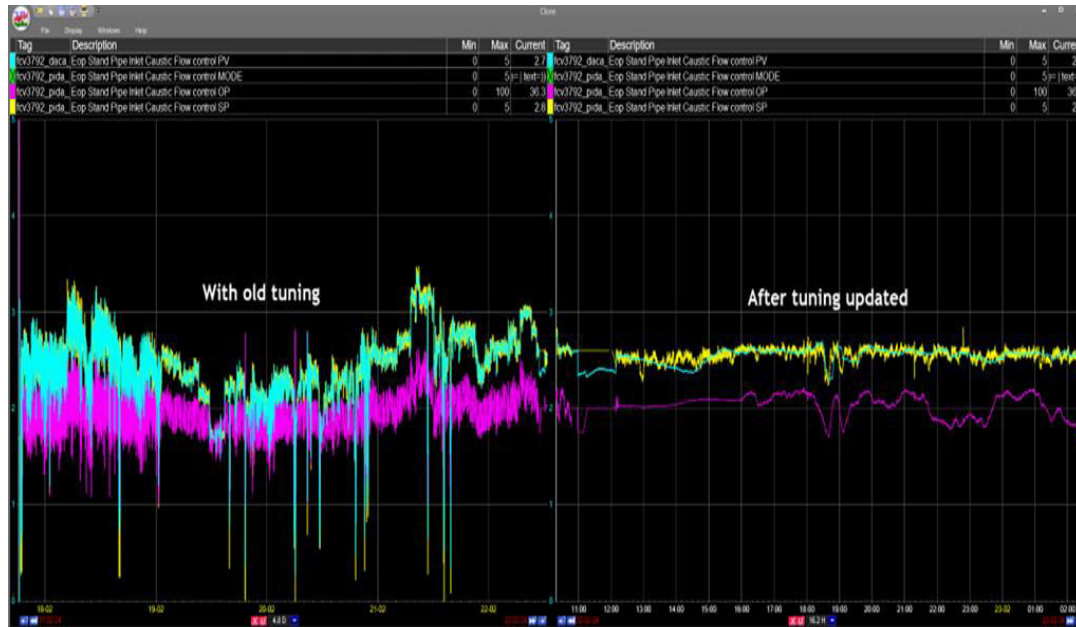
Advanced control strategies

- Integration of Feedforward & Feedback control



Results from Loop Tuning ,Analytics, Loop Analytics

- Effective regulatory loop tuning ensures that control loops are responsive and stable.
- Implementing the recommended tuning parameter adjustments has significantly improved the stability of control loops important for MACSbleach control.



L1: Measurement

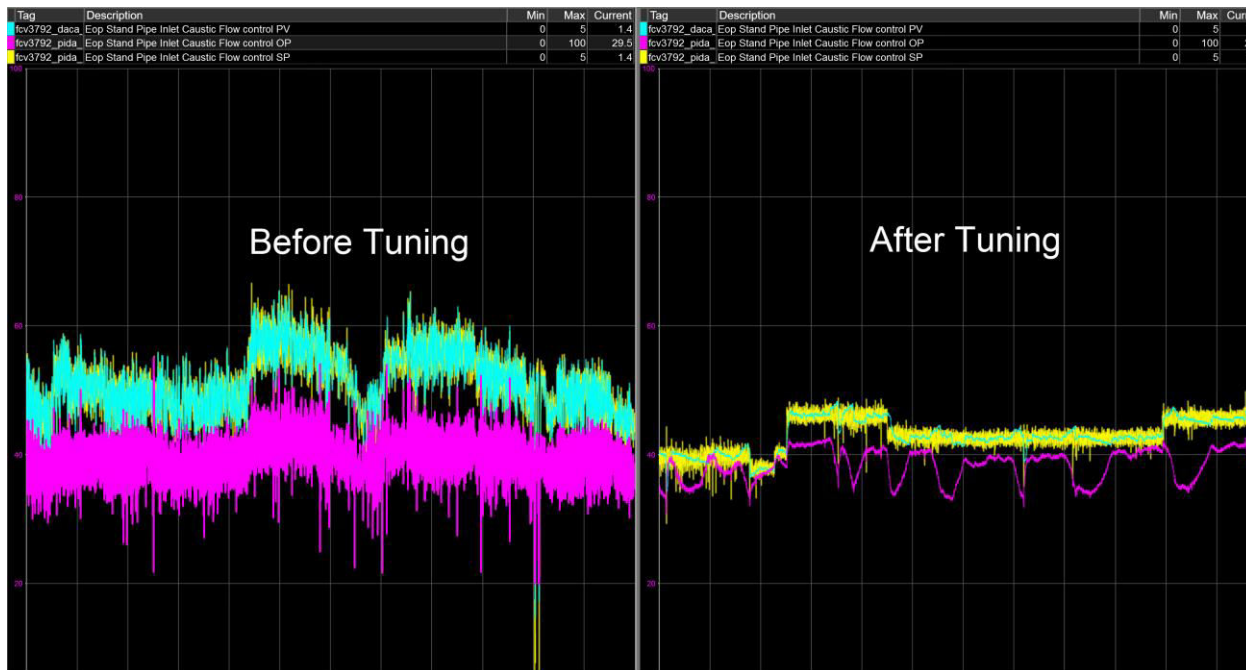
L2: Analytics

L3: APC

L4: Optimization

System Online - Model Improvements and Tuning

- Dynamics limit based on Kappa factor for D0 ClO2, to address the sudden swings in incoming kappa.
- Eop NaOH to outlet pH control, key improvement was using Eop filtrate pH in controls.
- D1 feed forward and feedback control to achieve maximum variability reduction in Final Brightness.
- D1 Acid Control, no online pH measurement, used D1 ClO2 & Eop Filtrate pH as feedforward and D1 vat pH (lab) as feedback signal.



The screenshot shows a process control software interface with several panels:

- Model Predictive Control:** Displays a log of events and control actions, including "Holding set value for D0_BLT" and "Est Quality received from DCl tag MV".
- Controlled Variables:** A table showing the status of various control loops.

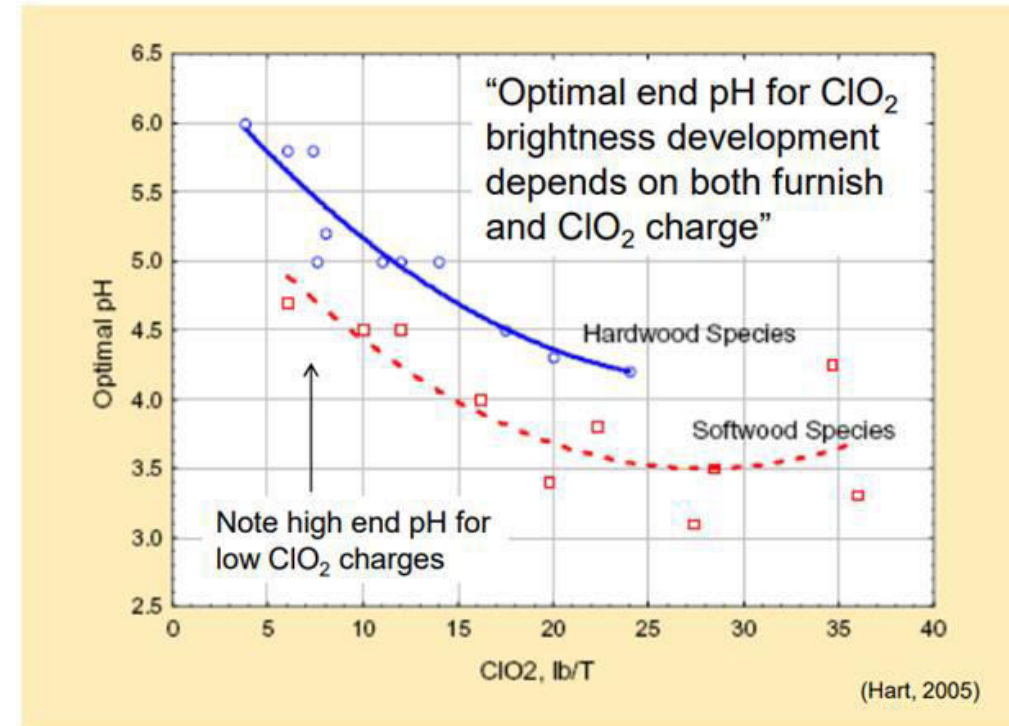
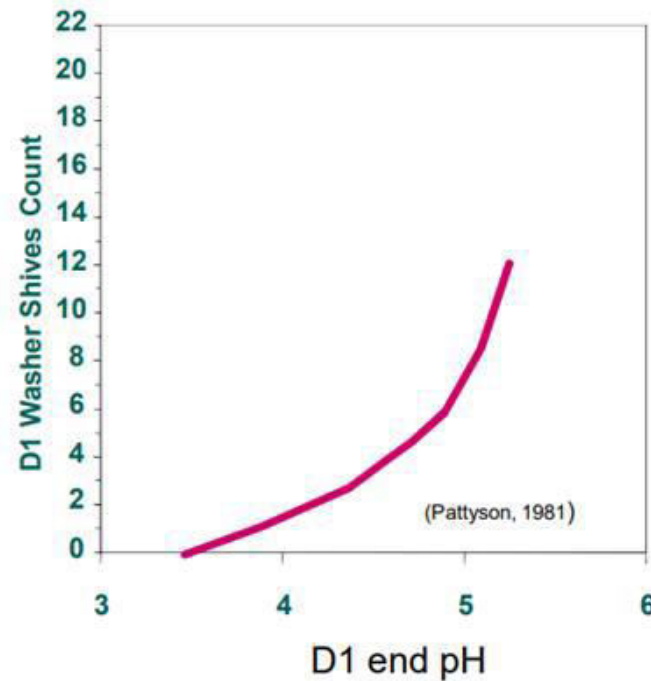
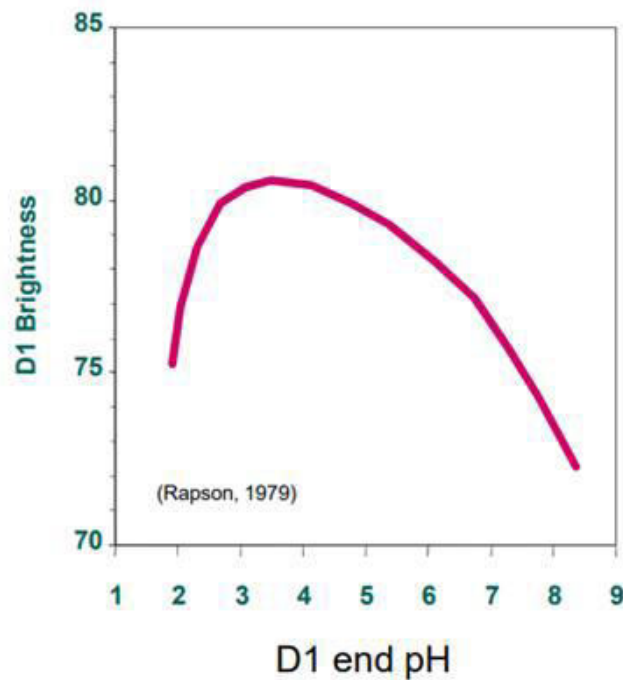
Tag/Name	Description	PV	On/Off	Status
D1_BR_OUT	D1 BR Outlet	86.773	ON	GOOD
D0_pH_IN	D0 Inlet pH	2.70939	ON	GOOD
Eop_pH_IN	Eop Inlet pH	11.7947	ON	GOOD
- Manipulated Variables:** A table showing the status of manipulated variables.

Tagname	Description	LocalSP	DCSMode	Status
D0_CIO2	D0 ClO2 (kg)	10.0988	REMOTE	GOOD
D0_H2SO4	D0 H2SO4 ()	18.6722	REMOTE	GOOD
Eop_NaOH	Eop NaOH ()	10.7161	REMOTE	GOOD
Eop_H2O2	Eop H2O2 ()	16.3195	REMOTE	GOOD
Eop_O2	Eop O2 (kg)	5	LOCAL	GOOD
D1_CIO2	D1 ClO2 (kg)	1.97819	REMOTE	GOOD
D1_H2SO4	D1 H2SO4 ()	3.89897	REMOTE	GOOD
D0_CIO2_Offset	D0 ClO2 Of	-12.8561	REMOTE	GOOD
D0_H2SO4_Offset	D0 H2SO4 ()	20.1960	REMOTE	GOOD
D1_CIO2_Offset	D1 ClO2 Of	21.7027	REMOTE	GOOD
D0_pH_IN_MV	D0 Inlet pH	2.43812	REMOTE	GOOD
Eop_pH_IN_MV	Eop Inlet pH	11.5552	REMOTE	GOOD
Tuning_D0_CIO2	RATE-slope	0	LOCAL	GOOD
Tuning_D1_CIO2	RATE-slope	0	LOCAL	GOOD
Tuning_D0_H2SO4	RATE-slope	0	LOCAL	GOOD
- Feedforward Variables:** A table showing the status of feedforward variables.

Tagname	Description	PV	On/Off	Status
EOP_OUT_PH_SWS	EOP Outlet pH	12.5206	ON	ISD
EOP_OUT_PH2_SWS	EOP Outlet pH	11.1677	ON	ISD
D1_OUT_PH_SWS	D1 Outlet pH	4.6570	ON	ISD
D1_IN_BR_SWS	D1 Inlet Br	78.923	ON	ISD
D1_OUT_BR_SWS	D1 Outlet Br	86.687	ON	ISD
D1_BR_IN_RAW	D1 Inlet Br	77.904	ON	ISD
D1_BR_OUT_RAW	D1 Outlet Br	86.694	ON	ISD
D1_BR_IN_VALMET	D1 Inlet Br	87.069	ON	ISD
EOP_PH_OUT_LABA	EOP pH Out	10.7564	ON	ISD
EOP_Filtrate_pH	Eop Filtrate	10.4904	ON	ISD
EOP_OUT_PH3_SWS	EOP Outlet pH	10.9944	ON	ISD

Optimizing pH for Bleaching Effectiveness

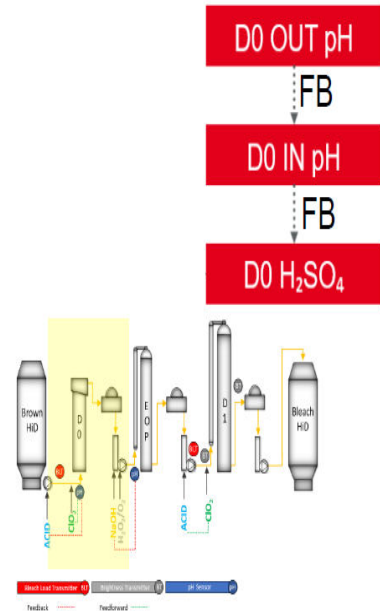
- The crucial role of pH in each stage.
- Acid and caustic stage
- Graph showing the optimal pH range for different stages.



Tailored Control for Each Bleaching Stage

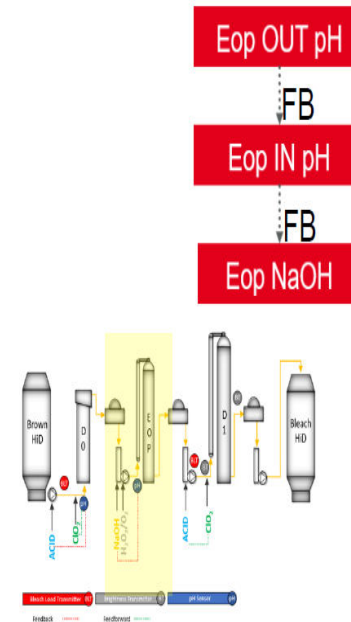
CTRL and Projection Models (FB) Only Projection Model (FF)		MV
		DO H ₂ SO ₄
CT/CVs	D0 Tower Inlet pH	-
	D0 Tower outlet pH (lab)	-

- D0 stage**



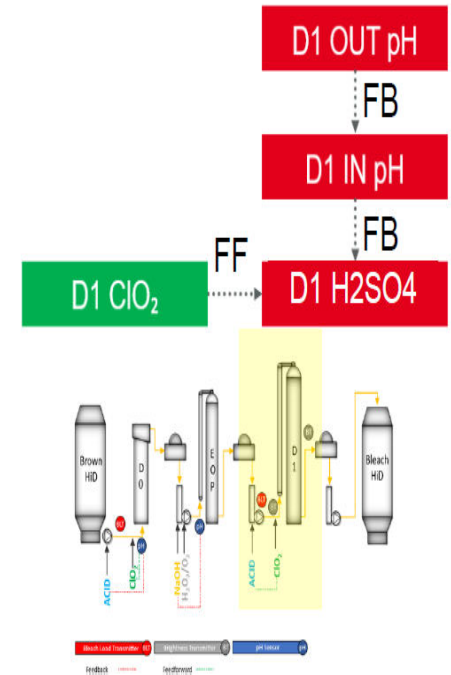
CTRL and Projection Models (FB) Only Projection Model (FF)		MVs	
		Eop NaOH	Outlet pH Target
CT/CVs	Eop inlet pH	+	
	Eop outlet pH		+

- EOP stage**



CTRL and Projection Models (FB) Only Projection Model (FF)		MV	FFs
		D1 H ₂ SO ₄	D1 ClO ₂
CT/CVs	D1 Tower Inlet pH	-	-
	D1 Tower outlet pH (lab)	-	-

- D1 stage**



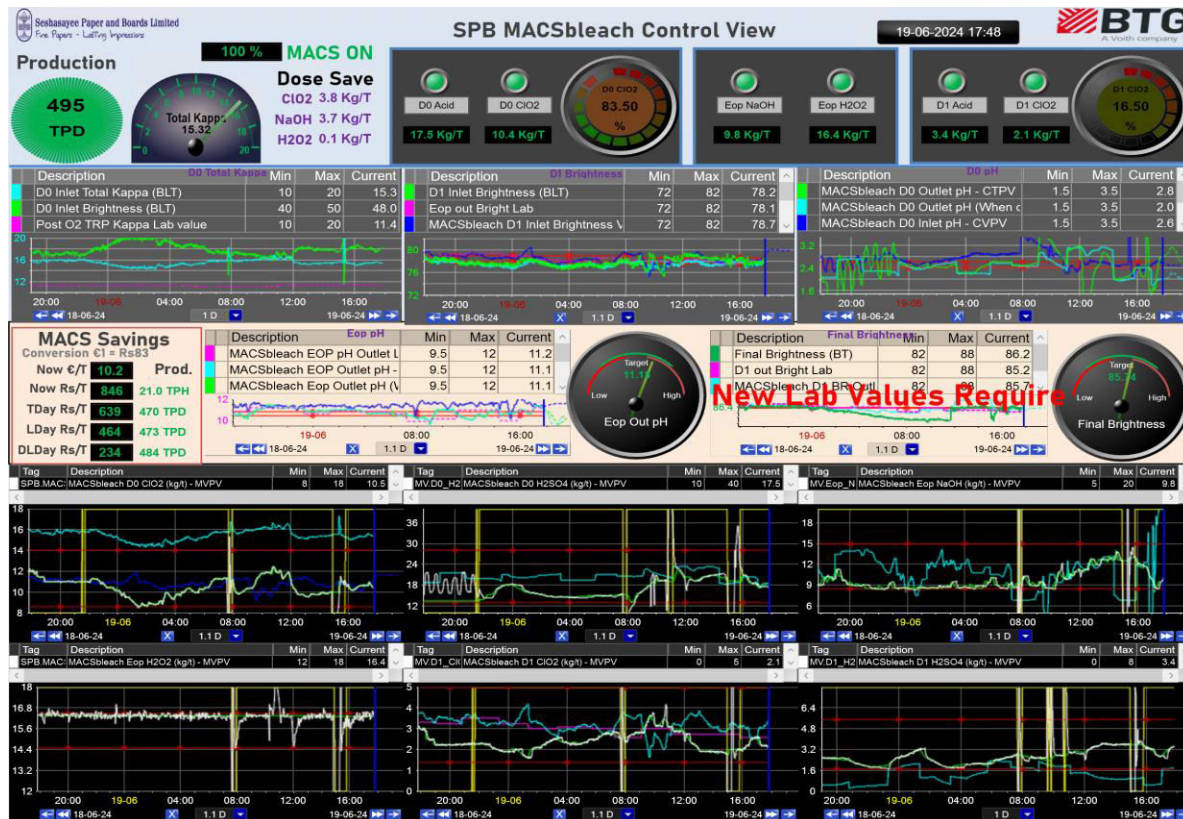
Leveraging SWS for Enhanced Control

- When sensors such as pH, Brightness sensors are coated, the values provided by the soft sensor become even more important.
- The soft sensor values are generated based on data entered by the operator, and the system automatically adjusts according to the programmed AI conditions



Dashboard & Trends

- Dashboard & Trends are available in Operator Control Room.
- Operators can see the future predictions for MVs and CVs on trends.



Real-time Visualization and Dashboard



BTG CONTROLS



[INDEX](#) | [BS WASHING](#) | [SCR & BSW#4](#) | [ODL1&2 SYS](#) | [PO 1 & 1A](#) | [TRP](#) | [DO_BLEACHIN](#) | [EOP BLEACHIN](#) | [D1 BLEACHING](#) | [WLO](#) | [CHE. HAND.SY](#) | [SEALNG WATE](#) | [TOTALIZERS](#)

MASTER ON

BTG FIRST OUT

CONTROL READY

WDOG

PROCESS VARIABLES		ON / OFF			PV (Kg/T)	SP (Kg/T)	STEADY STATE	SP MIN	SP MAX	WINDUP	LAST MOVE
● D0 ClO2	PI	BTG	DCS	CAS	11.12	10.58	10.60	10.50	13.80		0.00
● D0 H2SO4	PI	BTG	DCS	CAS	19.68	20.09	20.09	20.00	28.00		0.00
● Eop NaOH	PI	BTG	DCS	CAS	11.87	11.37	11.34	10.50	15.00		-0.01
● Eop H2O2	PI	BTG	DCS	CAS	18.97	19.00	19.00	16.00	18.50		0.00
● D1 ClO2	PI	BTG	DCS	CAS	3.76	3.71	3.71	1.80	3.80		-0.00
● D1 H2SO4	PI	BTG	DCS	CAS	3.18	3.09	3.09	3.00	5.50		0.00

CONTROLLED VARIABLES	ON / OFF	PV	STEADY STATE	PV MIN	TARGET	PV MAX	WINDUP
D0 Inlet pH	ON	2.61	2.62	2.40	2.74	2.80	
D0 Outlet pH	ON	2.40	2.40	2.40		2.80	
Eop Inlet pH	ON	10.93	11.11	10.50	11.11	11.30	
Eop Outlet pH	ON	10.70	10.67	10.50		10.90	
D1 Outlet pH	ON	4.10	4.10	4.00		4.50	
D1 Inlet Brightness	ON	77.20	77.81	75.80		77.20	
D1 Outlet Brightness	ON	84.49	84.72		85.80		

LAB VALUE MANUAL ENTRY		
	TIME	LAB_VALUE
TRP kappa	2.30	12.40
D0 pH VAT	10.30	2.40
Eop pH VAT	10.30	10.70
D1 pH VAT	10.30	4.10
ClO2 Strenght	6.00	8.00
NaOH Strenght	6.30	120.00
D0 out Bright	10.30	61.80
EOP out Bright	10.30	79.00
D1 out Bright	10.30	86.00

FFPV

D0 IN Kappa	15.00
D0 IN BR	47.83
D1 IN Kappa	4.29

PULP SHADE SELECTION FOR BTG

NORMAL SHADE

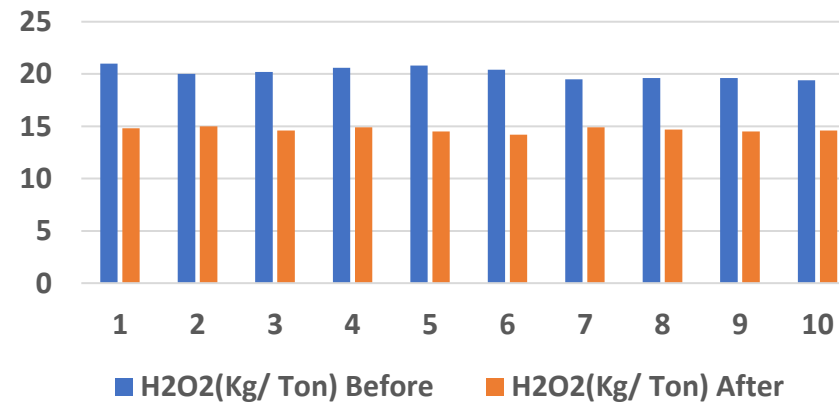
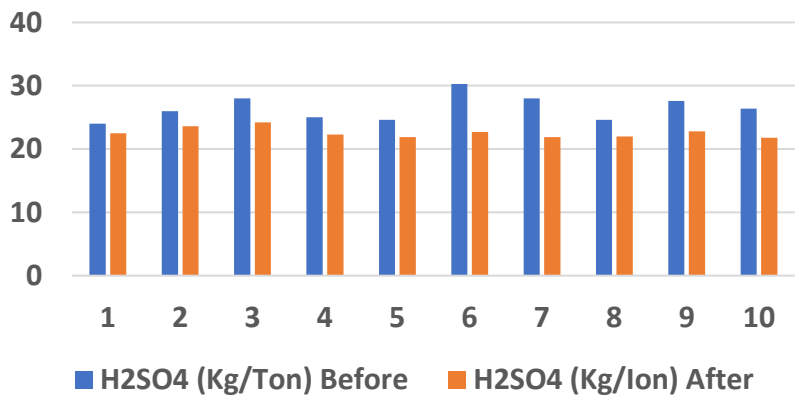
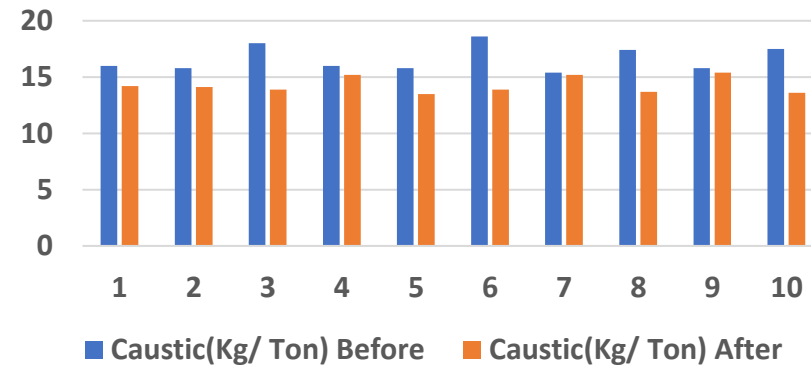
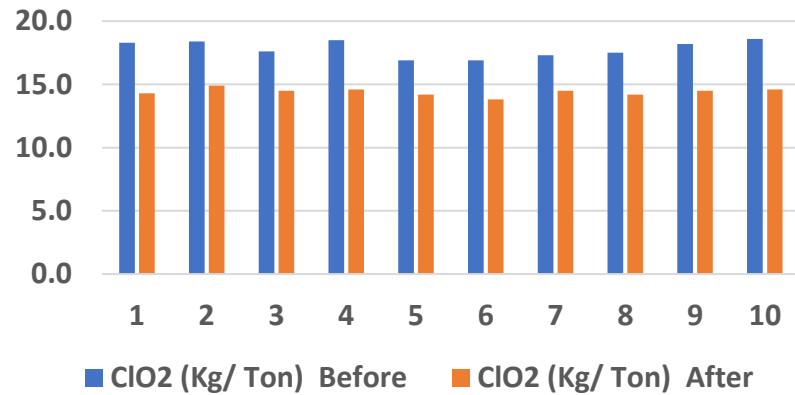
NATURAL SHADE

Overall Performance

Monthly KPI															
	Units	Jan-24	Feb-24	Mar-24	Apr-24	May-24	Jun-24	Jul-24	Aug-24	Sep-24	Oct-24	Nov-24	Dec-24	Jan-25	This year
General															
Production	adt/d	-	-	459	468	473	475	463	471	479	416	417	395	432	454
Process uptime	%	-	-	95%	94%	93%	94%	91%	94%	95%	61%	67%	63%	87%	85%
MACS uptime	%	-	-	19%	87%	88%	82%	72%	85%	73%	69%	70%	60%	62%	70%
Kappa & Brightness															
D0 inlet Kappa	Kappa	-	-	12.1	12.3	12.1	11.8	11.6	11.7	11.2	11.2	11.8	12.1	11.6	11.8
D1 inlet Brightness	%ISO	-	-	76.2	77.5	77.7	77.9	77.8	77.9	78.1	77.6	77.8	77.8	78.0	77.7
Final Brightness (LAB)	%ISO	-	-	85.6	85.3	85.7	85.8	85.8	85.5	85.6	85.2	85.2	85.3	85.5	85.5
Final Brightness (SWS)	%ISO	-	-	84.5	85.4	85.7	85.8	85.8	85.5	85.6	85.2	85.3	85.4	85.5	85.5
pH															
D0 inlet pH	pH	-	-	2.5	2.7	2.6	2.7	2.8	2.7	2.6	2.6	2.5	2.7	2.6	2.6
D0 outlet pH	pH	-	-	2.4	2.5	2.5	2.6	2.5	2.5	2.4	2.5	2.5	2.5	2.4	2.5
Eop Inlet pH	pH	-	-	11.3	11.1	11.4	11.4	11.3	11.4	11.8	11.8	12.2	11.9	12.1	11.6
Eop outlet pH	pH	-	-	11.0	10.8	10.5	10.6	10.7	10.4	10.6	10.8	10.6	10.6	10.7	10.6
D1 outlet pH	pH	-	-	6.8	4.3	3.9	3.8	4.1	4.1	4.6	4.3	4.2	4.1	4.4	4.3
Chemical Dosage															
Total ClO2	kg/adt	-	-	15.8	15.0	14.2	15.0	14.7	15.1	15.7	16.2	16.6	16.1	16.1	15.3
Total ClO2 (baseline)	kg/adt	-	-	16.6	16.5	16.5	16.4	16.4	16.4	16.3	16.3	16.4	16.5	16.4	16.4
Total NaOH	kg/adt	-	-	12.0	11.0	9.7	9.9	10.1	12.2	11.6	11.7	12.2	12.5	12.4	11.2
Total NaOH (baseline)	kg/adt	-	-	14.4	14.3	14.1	13.9	13.8	13.8	13.3	13.4	13.9	14.1	13.8	13.9
Total H2O2	kg/adt	-	-	18.2	16.0	15.0	15.9	14.9	14.9	16.1	15.7	15.3	15.2	15.1	15.5
Total H2O2 (baseline)	kg/adt	-	-	16.0	16.0	15.9	15.9	15.9	15.9	15.8	15.8	15.9	15.9	15.9	15.9
Total H2SO4	kg/adt	-	-	25.7	21.7	21.4	18.7	18.5	24.5	21.9	26.2	31.3	29.4	28.9	23.5
Total H2SO4 (baseline)	kg/adt	-	-	21.6	21.1	19.8	18.7	17.7	18.1	16.3	16.9	18.7	19.9	18.2	18.7
Savings															
ClO2 savings	€/adt	-	-	1.57	3.39	4.94	3.15	3.78	2.90	1.26	0.30	-0.36	0.76	0.62	2.42
NaOH savings	€/adt	-	-	1.21	1.67	2.23	1.99	1.83	0.80	0.85	0.87	0.84	0.79	0.69	1.34
Total savings	€/adt	-	-	2.78	5.06	7.17	5.14	5.61	3.70	2.11	1.17	0.48	1.55	1.31	3.76
Monthly savings	€/Month	-	-	37363	67012	97370	68664	72959	51067	28623	9199	4047	11954	15217	42134
Control usage (MV ON)															
DO ClO2	%	-	-	24%	96%	96%	95%	94%	96%	97%	84%	86%	75%	90%	85%
DO H2SO4	%	-	-	26%	94%	96%	95%	93%	97%	97%	83%	71%	68%	82%	83%
Eop NaOH	%	-	-	26%	92%	92%	91%	75%	90%	78%	77%	78%	75%	72%	77%
Eop H2O2	%	-	-	25%	92%	93%	98%	94%	94%	53%	63%	73%	69%	80%	76%
D1 ClO2	%	-	-	20%	94%	91%	88%	93%	94%	93%	77%	80%	68%	80%	80%
D1 H2SO4	%	-	-	21%	96%	93%	89%	85%	81%	11%	6%	10%	4%	7%	50%

ClO2 ,H2SO4,NaOH and H2O2 - Before and after 10 months data

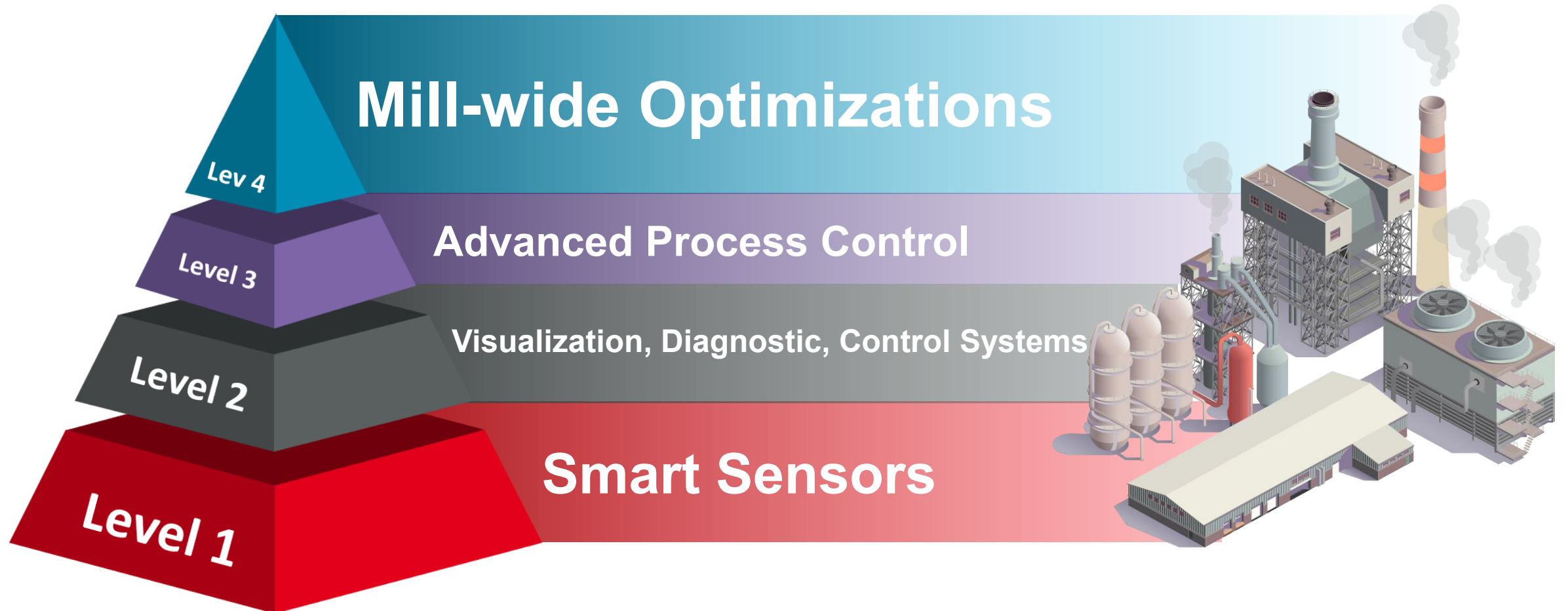
- Bar graph showing chemical usage before and after.



Benefits Achieved

- ClO₂ : Reduction in consumption by 1.0 Kg/Ton Savings
- Caustic: Reduction in consumption by 1.2 Kg/Ton Savings
- Acid: High Scope for reduction by adjusting the D0 inlet pH.
 - Need to find the optimum pH to avoid the scaling issue in D0 Washing
- Additional Benefits:
 - Reduction in Paper Machine OBA is an additional cost benefit
 - GHG emission:
 - 1 kg of ClO₂ -> 1.56 kg of CO₂
 - 1 kg of NaOH-> 1.35 kg of CO₂

Roadmap to Sustainable Optimization



Artificial intelligence is not a substitute for human intelligence;
“It is a tool to amplify human creativity and ingenuity.”



Proud to be a Responsible Paper Maker

Thank You