Enzyme Pre-Bleaching Towards ECF Pulp: A Successful Attempt at Century Pulp and Paper

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ABSTRACT

With the focus shifting towards Cleaner Production options in terms reduction of Chlorine in the Bleaching Process and subsequently minimal AOX levels in effluent discharges, Century Pulp and Paper conducted detailed studies on Enzyme Prebleaching to ascertain it's effectiveness. The positive results led to successful adoption of 'Bio Bleaching' for different durations in all the three fibre lines the company operates, particularly in Bagasse based pulping where "Elemental Chlorine Free" pulp could be produced with excellent results.

An Alkaline hemicellulase (Xylanase) enzyme was put to optimum use as a Bleach Boosting agent. Enzyme selectively removes xylan from the surface and the pores of the fibres, which facilitates the subsequent bleaching, reducing the bleaching chemicals required to reach the same degree of delignification.

The paper outlines the findings of the pilot and plant scale trials conducted with the enzyme and benefits derived in terms of Enhanced brightness of pulp with lower bleaching chemicals and reduction in AOX levels in the discharged effluents.

INTRODUCTION

Mounting environmental pressure and awareness has led the Paper Industry to look for Cleaner Production options in terms of reduced consumption of chlorine and it's compounds in the bleaching sequences thereby minimising the discharge of chlorinated organics in the effluent i.e. A.O.X. Century Pulp and Paper, adopting a pro-active approach, experimented with enzyme prebleaching for its three fibre lines with an objective to reduce the lignin content entering the bleach plant, Though enzyme usage as bleach boosting agent has been widely discussed in recent past, it's commercial viability was yet to be fully established. Based on the successful pilot scale studies conducted, Century Pulp and Paper adopted the new technology for its different fibrelines for varying durations to good effect and has been able to establish an ECF bleaching sequence for it's Bagasse based plant.

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ENZYME PREBLEACHING

A close interaction and further studies in collaboration with supplier has resulted in development of an improved enzyme product that requires lower dosage without affecting the cost and guality of the treatment process. Century Pulp and Paper is an integrated pulp and paper unit having three fibre lines with installed capacities of 31320 TPA Rayon Grade Pulp, 37250 TPA Writing and Printing paper based on Eucalyptus and 84600 TPA Bagasse based paper plant.

| | | Annexu | ire : I | | | |
|-----------------------|-----------|--|------------------|-----------------------|--------------|---------|
| Effect of Enzy | me on ble | achability of | WPP pulp | under differen | t conditions | |
| | each pulp | Kappa No. Brightness Viscosity CED Soln.) | : % : cP : | 18.84 34.4 12.7 | | |
| | (0.070 | Effect | of pH | | | |
| Set No | : | Ι | II | III | IV | v |
| Pulp Consistency % | : | 10 | 10 | 10 | 10 | 10 |
| Enzyme Doses gm/tonne | : | х | 500 | 500 | 500 | 500 |
| Retention Time, mints | : | 60 | 60 | 60 | 60 | 60 |
| Temperature °C | : | Ambient | Ambient | Ambient | Ambient | Ambient |
| pH | | 8.0 | 6.0 | 7.0 | 8.0 | 9.0 |
| Kappa No. | : | 18.84 | 18.0 | 18.64 | 17.28 | 17.06 |
| Brightness % | : | 34.4 | 35.2 | 35.0 | 35.2 | 35.4 |
| Viscosity cP | : | 12.7 | 13.6 | 13.55 | 13.4 | 13.2 |
| (0.5 % CED Soln.) | | | | | | |
| • | | Effect of | of Doses | | | |
| Set No | : | I | II | 111 | IV | V |
| Pulp Consistency % | : | 10 | 10 | 10 | 10 | 10 |
| Enzyme Doses gm/tonne | : | 300 | 400 | 500 | 600 | 700 |
| Retention Time, mints | : | 60 | 60 | 60 | 60 | 60 |
| Temperature °C | : | Ambient | Ambient | Ambient | Ambient | Ambient |
| pH | : | 8.5 | 8.5 | 8.5 | 8.5 | 8,5 |
| Kappa No. | : | 17.93 | 17.39 | 16.92 | 16.40 | 16.24 |
| Brightness % | • | 35.0 | 34.7 | 35.3 | 34.9 | 35.4 |
| Viscosity cP | : | 13.9 | 13.7 | 13.7 | 13.6 | 13.5 |
| (0.5 % CED Soln.) | | | | | | |
| | | <u>Effect of T</u> | emperature | _ | | |
| Set No | : | I | II | III | IV | V |
| Pulp Consistency % | : | 10 | 10 | 10 | 10 | 10 |
| Enzyme Doses gm/tonne | : | 500 | 500 | 500 | 500 | 500 |
| Retention Time, mints | : | 60 | 60 | 60 | 60 | 60 |
| Temperature °C | : | Ambient | 40 | 50 | 60 | 70 |
| рН | : | 8.5 | 8.5 | 8.5 | 8.5 | 8.5 |
| Kappa No. | • | 16.92 | 16.72 | 16.64 | 17.12 | 17.44 |
| Brightness % | • | 35.3 | 35,3 | 35.1 | 35.0 | 35.0 |
| Viscosity cP | : | 13.7 | 14.3 | 14.05 | 14.0 | 14.05 |
| (0.5 % CED Soln.) | | | | | | |

BACKGROUND

During the bleaching process, a significant amount of Organic material is dissolved in Chlorination and Extraction stage When Chlorine is extensively used for bleaching, an appreciable quantity of Organically bound Chlorine finds it's way in the effluent, reported as Adsorbable Organic Halides (AOX). In view of the proposed revision of the limit for this parameter, it becomes imperative that necessary corrective steps are taken to minimise this load.

Enzyme Pre bleaching using Xylanase enzymes offers a solution by improving the effectiveness of conventional Bleaching chemicals in removing Lignin. Xylanase enzymes are reported to partially hydrolyse the hemi-cellulase portion of pulp. The enzyme is presumed to hydrolyse Xylan into smaller fragments allowing lignin associated with these short hemicellulose chains to be more easily removed through subsequent Extraction stages in bleaching.

EXPERIMENTAL

Detailed experimentations with both Wood and Bagasse pulps were conducted to ascertain the effectiveness of bleach boosting enzyme. During the lab studies, effect of Pulp Consistency, Retention Time, Enzyme Dosage, Temperature and pH were particularly monitored and optimised. The effect of these parameters on unbleached pulp (WPP) are depicted in Annexure 1 based on which the optimal Conditions were found as ;

| | | Annes | ure : II | | | | |
|----------------------------------|-------------|-----------------|-----------------|--------|--------|-----------------|--------|
| Bleaching of Enzyme treated pulp | | | | | | | |
| Bleaching Sequences | : | | | | | | |
| Set No | : | I | II | III | | IV | v |
| | | Nil | Enzyme | Enzyme | | Enzyme | Enzyme |
| | | C / D | C / D | C / D | 1 | C / D | C / D |
| | | E/ P | E / P | E | • | Е/Р | E |
| | | НуроІ | HypoI | Hypol | [| НуроІ | Hypol |
| | | HypoII | HypoII | Hypoll | | | ~~ • |
| | | D | D | D | | D | D |
| | | SO ₂ | SO ₂ | SO | 2 | SO ₂ | SO |
| Properties | | | | | | | |
| Brightness (ISO) | % : | 86.7 | 87.7 | 87.2 | 2 | 87.6 | 88.1: |
| P. C. No | : | 0.23 | 0.21 | 0.21 | | 0.19 | 0.1 |
| Yellowness | % : | 4.67 | 3.86 | 3.87 | 7 | 3.49 | 3.4 |
| L | : | 96. 4 7 | 96.09 | 95.69 |) | 95,60 | 96.4 |
| а | • | - 0.4 | - 0.4 | - 0.4 | k s | - 0.4 | - 0.4 |
| b | : | 2.6 | 2.2 | 2.1 | l | 2.0 | 2. |
| Viscosity | cP : | 3.94 | 4.07 | 4.26 | | 4,55 | 4.7 |
| (0.5% CED | | | | | | | |
| | Addition o | | and Condition | | - | | |
| | | C / D | E / P | Hypol | HypoII | D | SO |
| Chemical | %: | 3.0 | 2.0 | 2.0 | 0.5 | 0.5 | 0.1 |
| | | 0.15 | 0.5 | | | | |
| Retenton Tin | | 45 | 90 | 90 | 90 | 180 | 1: |
| Temp. | °C : | Ambient | 60-65 | 40-42 | 40-42 | 70-75 | Ambien |

| | | | Annex | ure : III | | | | |
|----------------------------------|------------|-----------------|----------------------|------------------|-----------------|-----------------|-----------------|------------|
| | | 1 | Bio Bleaching | of Bagass | se Pulp | | | |
| | | Unbleach pul | p sample coll | ected fron | n unbleach | thickner | | |
| Condition of | | | | | | | | |
| | | Doses : | 0.05 % | | | | | |
| | Ret | ention time : | 60 mints | | | | | |
| | | Temp : | Ambient | | | | | |
| | | pH : | 8.5 | | | | | |
| | | As such | | | - | yme Treatmen | it | |
| Kapj | pa No. | : | 10.98 | | | 9.54 | | |
| Brig | htness | %: | 49.60 | | | 0.10 | | |
| Visc | osity | cP : | 20.98 | | 2 | 1.76 | | |
| | | E | Bleaching Exp | eriment | | | | |
| | | | Set No. | | | | | |
| With | nout enzy | me < | (| • | Enzyme T | reated Pulp | | > |
| Trea | tment. | | | | | | | |
| | | 1 | ŀ | l | 1 | 1 | | I |
| | * | * | * | * | * | * | * | * |
| 1 | Normal | ECF | ECF | ECF | ECF | ECF | ECF | ECF |
| | I | II | Ш | IV | V | VI | VII | VIII |
| | C/D | D | D | D | D | D | D | D |
| | E/P | E/P | E/P | E/P | E/P | E/P | E/P | E/P |
| | D | D | D | D | D | D | D | D |
| | SO, | SO ₂ | SO ₂ | SO ₂ | SO ₂ | SO ₂ | SO ₂ | SO, |
| Chemical Add | | 2 | 2 | - | - | - | - | _ |
| Ist Stage | | | | | | | | |
| Cl , % : | 2.0 | - | - | - | - | - | - | - |
| ClO_{2} % : | 0.5 | 0.5 | 0.5 | 0.5 | 0.5 | 0.5 | 0.5 | 0.5 |
| $H_2SO_4 \%$: | | 0.5 | 0.5 | 0.5 | 0.5 | 0.5 | 0.5 | 0.5 |
| IInd Stage | | | | | | | • • | • • |
| NaOH % : | 2.0 | 2.0 | 2.0 | 2.0 | 2.0 | 2.0 | 2.0 | 2.0 |
| H ₂ O ₂ %: | 0.5 | 0.5 | 0.5 | 0.5 | 0.75 | 0.75 | 1.0 | 1.0 |
| IIIrd Stage | | | . . | 6 F | | 0.E | 07 | 0.7 |
| C1O ₂ % : | 0.5 | 0.5 | 0.5 | 0.5 | 0.7 | 0.5 | 0.7 | 0.7 |
| $H_2SO_4 \%$: | 0.5 | 0.5 | 0.5 | 0.5 | 0.5 | 0.5 | 0.5 0.2 | 0.5 0.2 |
| SO ₂ %: | 0.2 | 0.2 | 0.2 | 0.2 | 0.2 | 0.2 | | |
| Br. % : | 88.1 | 84.7 | 85.9 | 86.8 | 85.4 | 86.7 | 86.8 | 87.8 |
| (ISO) | 0.1 | 0.40 | 0.24 | 0.27 | 0.29 | 0.24 | 0.21 | 0.19 |
| P. C. No. : | 0.1 | 0.48 | 0.34 17.2 | 0.27 16.9 | 17.2 | 17.4 | 17.5 | 17.3 |
| Vis. cP : | 17.6 | 16.90 | 11.4 | 10.7 | 17.4 | 11.7 | 17.5 | .,,, |
| (0.5% CED) | 2 40 | 4.79 | 3.97 | 3.90 | 3.79 | 3.80 | 2.96 | 2.70 |
| Yell. % : | 2.49 | | ime (Mints) | Temp. | | pH | | 2.70 |
| | | Normal / | ECF | - | I / ECF | - | lormal | ECF |
| let Stage | | 45 | <i>2</i> 01 | | ib. 50-55 | - | 2.1 | 3.7 |
| Ist Stage IInd Stage | • | 120 | | | 60-65 | | 9.6 | 9.7 |
| IIIrd Stage | • | 120 | 150 | | 70-75 | | 3.8 | 3,9 |
| - | • • • | luced and brig | | tability im- | | HO treatmo | | |
| Yellowness (| iell.) fed | iuceu and orig | 11111055 (DI.) S | LAULILLY HILL | JIUYCA WILL | mo, ucaune | me withing OI | "Putticas |

| | | Ann | exure : IV | | | | |
|---|---|---|--------------------|--|----------------------|--|------------------------------------|
| | I | Bio Bleaching : | Dissolving | Grade Pul | p. | | |
| Un | bleach pulp | p sample collect | ed from un | bleached t | hickner (R | GP) | |
| Condition of Enzym | e Treatme | <u>nt</u> : | | | | | |
| | Dos | es: 0.05 % | | | | | |
| R | etention tin | ne: 60 mints | | | | | |
| | Ten | np: Ambient | | | | | |
| | р | H: 8.5 | | | | | |
| | | As such | | After Enz | zyme Treati | nent | |
| Kappa No. | | 12.62 | | | 11.52 | | |
| Brightness | %: | 32.1 | | | 33.90 | | |
| Viscosity | cP : | 10.6 | | | 0.80 | | |
| Bleaching condition | | | | | | | |
| Three set were cond | | eaching | | | | | |
| a: Without enzyme t | | - | 1 | | | | |
| a. Without chaying t | reatment (1) | vormai sequence) | | | | | |
| • | tmant (Nor | mal coguanaa) | | | | | |
| b: With enzyme trea | | • | | | | | |
| b: With enzyme trea | | • | | | | | |
| b: With enzyme trea c: With enzyme trea | tment (Hype | • | | | | | |
| b: With enzyme trea c: With enzyme trea <u>Bleaching</u> <u>Sequence</u> | tment (Hype | • | E | <u>Hypol</u> | <u>HypoII</u> | <u>Dioxide</u> | <u>so</u> |
| b: With enzyme trea c: With enzyme trea | tment (Hype | o II eleminated) | <u>E</u> 2.8 | <u>Hypol</u> 2.0 | <u>НурсII</u> 0.5 | Dioxide | |
| b: With enzyme trea c: With enzyme trea <u>Bleaching Sequence</u> Chemical | tment (Hypo <u>s</u> <u>:</u> | o II eleminated) <u>C</u> | | | | | 0.40 |
| b: With enzyme trea c: With enzyme trea <u>Bleaching Sequence</u> Chemical Retn. Time, Mints | tment (Hypo <u>s</u> <u>:</u> | o II eleminated) <u>C</u> 3.2 | 2.8 | 2.0 | 0.5 | 1.0 | 0.40 30 |
| b: With enzyme trea c: With enzyme trea Bleaching Sequence Chemical Retn. Time, Mints Temp. | tment (Hypo <u>s</u> : %: C: | o II eleminated) <u>C</u> 3.2 60 | 2.8 90 | 2.0 90 | 0.5 90 | 1.0 180 | 0.40 30 |
| b: With enzyme trea c: With enzyme trea Bleaching Sequence Chemical Retn. Time, Mints Temp. | tment (Hypo <u>s</u> : %: C: | o II eleminated) <u>C</u> 3.2 60 Ambient | 2.8 90 60-65 | 2.0 90 40 | 0.5 90 42 | 1.0 180 75 -80 | 0.40 30 |
| b: With enzyme trea c: With enzyme trea Bleaching Sequence Chemical Retn. Time, Mints Temp. | tment (Hypo <u>s</u> : %: C: | o II eleminated) <u>C</u> 3.2 60 Ambient Set No. I | 2.8 90 60-65 | 2.0 90 40 Set No II | 0.5 90 42 | 1.0 180 75 -80 Set No III | 0.40 30 |
| b: With enzyme trea c: With enzyme trea <u>Bleaching Sequence</u> Chemical Retn. Time, Mints Temp. <u>Properties (Final Pu</u> | tment (Hypo <u>s</u> : %: C: | o II eleminated) <u>C</u> 3.2 60 Ambient Set No. I (a) | 2.8 90 60-65 | 2.0 90 40 Set No II (b) | 0.5 90 42 | 1.0 180 75 -80 Set No III (c) | 0.40 30 |
| b: With enzyme trea c: With enzyme trea <u>Bleaching Sequence</u> Chemical Retn. Time, Mints Temp. <u>Properties (Final Pu</u> Brightness | tment (Hypo <u>s</u> <u>:</u> % : : C : <u>ulp)</u> <u>:</u> | o II eleminated) <u>C</u> 3.2 60 Ambient Set No. I | 2.8 90 60-65 | 2.0 90 40 Set No II | 0.5 90 42 | 1.0 180 75 -80 Set No III | 0.40 30 |
| b: With enzyme trea c: With enzyme trea Bleaching Sequence Chemical Retn. Time, Mints Temp. Properties (Final Pu Brightness (ISO) | tment (Hypo <u>s</u> <u>:</u> % : : C : <u>ulp)</u> <u>:</u> | o II eleminated) <u>C</u> 3.2 60 Ambient Set No. I (a) | 2.8 90 60-65 | 2.0 90 40 Set No II (b) 88.70 | 0.5 90 42 | 1.0 180 75 -80 Set No III (c) 88.6 | 0.40 30 |
| b: With enzyme trea c: With enzyme trea Bleaching Sequence Chemical Retn. Time, Mints Temp. Properties (Final Pu Brightness (ISO) Yellowness | tment (Hypo <u>s</u> <u>:</u> % : <u>C</u> : <u>ulp) :</u> % : | o II eleminated) <u>C</u> 3.2 60 Ambient Set No. I (a) 87.10 3.93 | 2.8 90 60-65 | 2.0 90 40 Set No II (b) 88.70 3.78 | 0.5 90 42 | 1.0 180 75 -80 Set No III (c) 88.6 3.41 | 0.40 30 |
| b: With enzyme trea c: With enzyme trea Bleaching Sequence Chemical Retn. Time, Mints Temp. Properties (Final Pu Brightness (ISO) Yellowness P.C. No | tment (Hypo <u>s</u> <u>:</u> % : <u>:</u> % : <u>11p) : % : ; </u> | o II eleminated) <u>C</u> 3.2 60 Ambient Set No. I (a) 87.10 3.93 0.79 | 2.8 90 60-65 | 2.0 90 40 Set No II (b) 88.70 3.78 0.42 | 0.5 90 42 | 1.0 180 75 -80 Set No III (c) 88.6 3.41 0.3 | 0.40 30 |
| b: With enzyme trea c: With enzyme trea <u>Bleaching</u> <u>Sequence</u> | tment (Hypo <u>s</u> <u>:</u> % : <u>C</u> : <u>ulp) :</u> % : | o II eleminated) <u>C</u> 3.2 60 Ambient Set No. I (a) 87.10 3.93 | 2.8 90 60-65 | 2.0 90 40 Set No II (b) 88.70 3.78 | 0.5 90 42 | 1.0 180 75 -80 Set No III (c) 88.6 3.41 | <u>SO</u> 0.40 30 Ambient |

| Consistency | : | 10% |
|----------------|---|------------|
| Retention Time | : | 60 minute. |
| Temperature | : | Ambient |
| рН | : | 8.5 |

These conditions were tailored to suit the existing process facilities. Enzyme treated pulp was further bleached under various sequences to attain a brightness of 87.0% (+). The details of the bleaching and the

findings are shown in Annexure II. An increase in brightness by 1.5 points even after elimination of Hypo II stage was achieved, with reduction in yellowness and P.C. No.

For Bagasse pulp, attempts were made to achieve the required brightness by totally eliminating Elemental Chlorine (ECF) by supplimentation with Hydrogen peroxide in the Extraction stage.

The experimental details on the Bleachability of Bagasse Pulp with and without enzyme and further

| | Bio Bleac | Annexu hing with Imp | re : V roved Version E | Inzvmc | | |
|-------------------------------|--------------------|-------------------------|---------------------------|-----------------|-------|-----------------|
| | | (WPP | | | | |
| U | nbleach pulp | | ted from unblea | ch thickner | | |
| Condition of Enzyme T | | • | | | | |
| | gm/tonne : | 200 | 250 | 300 | | |
| Retent | ion time : | | 60 mints | | | |
| | Temp : | | Ambient | | | |
| | pH : | | 8.5 | | | |
| | As such | < Afte | r Enzyme Treatm | nent> | | |
| | Blank | 200 | 250 | 300 | | |
| Kappa No. : | 19.43 | 17.64 | 17.57 | 17.50 | | |
| Brightness % : | 26.5 | 26.9 | 26.8 | 26.8 | | |
| Viscosity cP : | 13.0 | 13.4 | 13.5 | 13.5 | | |
| 1 | Bleaching Exp | periment | | | | |
| | Set No. | | | | | |
| | < | | Enzyme Treated | Pu1p | > | |
| | Blank | 200 gm | 300 gm | 200 gm | | |
| Set No : | I | II | III | IV | (* | Chemical) |
| | | | | *** | (| (Addition) |
| | C / D | C / D | C / D | C / D | 2 | 2.0 + 0.15 |
| | E / P | E/P | E / P | E / P | 2 | 0 + 0.5% |
| | HypoI | Hypol | НуроІ | HypoI | | 2.0 % |
| | HypoII | HypoII | HypoII | | | |
| | D | D | D | D | | 0.5 % |
| | SO ₂ | SO, | SO ₂ | SO, | | 0.2 % |
| Brightness % : | 84.35 | 85.89 | 86.14 | 85.66 | | |
| (ISO) | | | | | | |
| P. C. No : | 0.77 | 0.36 | 0.33 | 0.46 | | |
| Viscosity cP : | 5.85 | 5.97 | 5.92 | 5.89 | | |
| (0.5 % CED) | | | | | | |
| Yellowness % : | 7.70 | 5.76 | 5.42 | 5.86 | | |
| | <u>Addition of</u> | | d conditions (Bl | <u>eaching)</u> | | |
| | | (*** Except | | | | |
| | C/D | E/P | HypoI | HypoII | D | SO ₂ |
| Chemical % : | 3.0 | 2.0 | 2.0 | 0.5 | 0.5 | 0.19 |
| | 0.15 | 0.5 | | | | |
| Retention Time mints : | 45 | 90 | 90 | 90 | 180 | 15 |
| Temp. °C : | Ambient | 60-65 | 50 | 55 | 75-80 | Ambient |

supplemention with chlorine-Dioxide and Hydogen Peroxide is as per Annexure III attached.

Similar studies with dissolving grade Pulp (Eucalyptus) fibre line are shown in Annexure IV attached.

As part of the recent development based on the

detailed experimentation on pilot and Plant scale, an improved version of the Enzyme Product has been developed with appreciable reduction in dosage i.e. from 500 gm/T ot 300 gm/T without any effect on cost/ quality. The details on this product are shown in Annexure V. as conducted on WPP (Wood based) fibre line. Further studies have been planned to try this product on wood based pulping section.

| Table : 1 | | | | | | |
|---------------------|------------------------|----------------|----|-----|--------|--|
| Plant trial details | of E n zyme | Prebleaching i | in | WPP | Street | |

| Particulars | | Without | With Enzy | ne |
|--|--|-----------|-----------|-----------|
| | | Enzyme | l | II |
| | Unbleached Pulp | | | |
| Enzyme gm/T | | 0 | 500 | 500 |
| Temp °C | | Ambient | Ambient | Ambient |
| Retention time min. | | 60 | 60 | 61 |
| рН | | 8.0-9.0 | 8.0-9.0 | 8.0-9.0 |
| Kappa No. | | 19.1-22.5 | 17.0-18.8 | 16.6-19.3 |
| ····· | Chlorine/Dioxide stage | | | |
| Cl ₂ % | | 2.5 | 2.5 | 2.5 |
| ClO ₂ % | | 0.34 | 0.34 | 0.34 |
| рН | | 2.0-3.0 | 2.0-3.0 | 2.0-3.0 |
| Kappa No. | | 9.8-11.9 | 6.8-7.3 | 6.7-7.6 |
| | Alkali Extraction/Perox | ide Stage | | l |
| NaOH % | | 1.1 | 1.1 | 1.1 |
| H ₂ O ₂ % | | 0.5 | 0.5 | 0.5 |
| pH | · · · · · · · · · · · · · · · · · · · | 9.5-10.5 | 9.5-10.5 | 9.5-10.5 |
| Kappa No. | | 8.0-9.3 | 4.9-5.3 | 4.7-5.6 |
| | Hypo I Stage | | | - |
| Hypo (as Cl ₂) % | · · · · · · · · · · · · · · · · · · · | 2.3 | 2.3 | 1.88 |
| рН | | 8.0-9.0 | 8.0-9.0 | 8.0-9.0 |
| | Hypo II Stage | | | |
| Hypo (as Cl ₂) % | | 1.75 | 1.75 | 0.66 |
| Brightness % | | 82.3-83.4 | 83.0-84.5 | 83.1-84.3 |
| рН | ······································ | 7.5-8.0 | 7.5-8.0 | 7.5-8.0 |
| ······································ | Chlorine Dioxide Stage | | J | |
| C10 ₂ % | | 0.2 | 0.2 | 0.2 |
| рН | | 3.0-5.0 | 3.0-5.0 | 3.0-5.0 |
| Brightness % | | 84.5-85.3 | 86.0-86.8 | 86.0-86.5 |
| Viscosity (0.5CED cP | | 4.0-4.44 | 4.9-5.1 | 5.05-5.15 |
| PC No. | | 1.0-1.14 | 0.5-0.69 | 0.44-0.62 |
| Yellowness % | | 5.17-6.39 | 2.9-4.0 | 2.6-3.9 |
| | Strength Properties at 3 | | | |
| Burst Factor | | 31 | 30 | 30 |
| Tear Factor | | 50 | 48 | 54 |
| Breaking length (meters) | | 4890 | 5070 | 5120 |
| Double Fold (No.) | · · · · · · · · · · · · · · · · · · · | 18 | 15 | 17 |
| In set-II, Hypo II was elim | inated and Hypo-In splitte | | | |
| @ 80:20 ratio. | | | | + |
| Additional Cost Rs/T | | | 350 | 200 |
| of Chemicals | | | | |

| Table : 11 | | | | | |
|---------------------|------------------------------------|----------|--|--|--|
| Plant trial details | s of Enzyme Prebleaching in Bagass | e Street | | | |

| Particulars | Without | | With Enz | yme |
|---------------------------------|---------------------------------------|-------------|------------|---|
| | Enzyme | I | II | III |
| | · · · · · · · · · · · · · · · · · · · | | ECF | ECF |
| Unl | pleached Pulp | | | |
| Enzyme gm/T | 0 | 500 | 500 | 500 |
| Temp. ^o C | Ambient | Ambient | Ambient | Ambient |
| Retention time, min. | 60 | 60 | 60 | 60 |
| рН | 8.0-9.0 | 8.0-9.0 | 8.0-9.0 | 9,0-9,0 |
| Kappa No. | 11.4-13.6 | 9.84-11.14 | 9.04-10.56 | 9.12-10.8 |
| Chl | orine/Dioxide stage | | | |
| Cl ₂ % | 2.2 | 1.5-1.6 | 0 | 0 |
| ClO ₂ % | 0.14 | 0.12-0.14 | 0.46 | 0.46 |
| pH | 1.0-1.8 | 1.5-2.0 | 1.5-2.0 | 1.5-2.0 |
| Kappa No. | 4.0-4.73 | 3.2-4.98 | 3.2-5.28 | 2.56-4.48 |
| Brightness % | 56-61 | 58-62 | 59-64 | 58-66 |
| All | ali Extraction/Oxygen | Stage | <u> </u> | ••••••••••••••••••••••••••••••••••••••• |
| NaOH % | 1.5 | 1.48 | 1.0-1.27 | 1.2 |
| O ₂ % | 0.4 | 0.4 | 0.4-0.5 | 0.4 |
| H ₂ O ₂ % | 0 | 0 | 0 | 0.27 |
| pH | 9.5-10.5 | 9.5-10.5 | 9.5-10.5 | 9.5-10.0 |
| Kappa No. | 1.19-1.68 | 1.2-1.84 | 0.96-1.42 | 0.72-1.60 |
| Brightness % | 68-72 | 67-72 | 74-78 | 75-85 |
| Ch | lorine Dioxide Stage | | | |
| C10, % | 0.46 | 0.46 | 0.45-0.48 | 0.49 |
| pH | 3.0-3.0 | 2.0-3.0 | 2.0-3.0 | 2.0-3.0 |
| Brightness % | 86.6-68.0 | 86.4-88.0 | 87.5-89.5 | 88.2-90.2 |
| Viscosity (0.5 CED) cP | 11.8-12.7 | 13.75-17.79 | 17.79-18.0 | 16.98-18.93 |
| PC No. | 0.24-0.42 | 0.16-0.30 | 0.12-0.30 | 0.12-0.30 |
| Yellowness % | 1.52-2.0 | 1.03-1.8 | 1.0-1.76 | 0.45-0.76 |
| Str | ength Properties at 35 | °SR | | - |
| Burst Factor | 30 | 31 | 32 | 32 |
| Tear Factor | 53 | 53 | 50 | 49 |
| Breaking length (meters) | 4980 | 4880 | 5050 | 5230 |
| Double Fold (No.) | 14 | 19 | 18 | 15 |
| Additional Cost Rs/T | - | 295 | 345 | 415 |
| of Chemicals | | | | |

RESULTS AND DISCUSSION

Based on the encouraging trends of pilot scale findings, Plant scale trials were undertaken. Enzyme was dosed at out let of Unbleached thickner @ 500 gm/

T after dilution. On line dilution arrangement was made as enzyme in diluted form is reported to be unstable. Retention time of at least 60 minutes and proper mixing with pulp are another factors considered for optimum results.

| AOX Levels in Effluents | | | | | | |
|-------------------------|------------------------|--------------------|--------------------|-------------|--|--|
| S. No. | Particulars | | AOX kgs/T | | | |
| | | Normal | Enzyme Treated | % Reduction | | |
| 1 | Writing Ptg Paper | 2.39 | 1.37 | 42.6 | | |
| | (Wood Based) | | | | | |
| | (Bleach Effluent) | | | | | |
| 2 | Bagasse Plant | 1.28 | 1.07 | 16.4 | | |
| | (Bleach Effluent) | | | | | |
| 3 | Final Discharge | 0.96 | 0.84 | 12.5 | | |
| | Results based on analy | sis carried out by | out side agencies. | | | |
| | CPP in the process of | equipment procur | rement) | | | |

Table : III

For Wood based fibre line during a month long trial maintaining the same bleaching chemicals, a Brightness improvement of 1.5 points was achieved. Further, Hypo II stage was eliminated i.e. 1.75% dose of Chlorine without affecting the quality of pulp. There was reduction in yellowness and P.C. Values. The details of the process conditions and results obtained are given in Table No.1

During the plant scale trials in bagasse bleaching , brightness could be maintained at the control levels with reduction of Chlorine to the tune of 7 kgs per tonne. Further experimentations by totally eliminating Chlorine with increased dosage of Chlorine dioxide and in second phase, introduction of Hydorgen Peroxide resulted in establishment of an ECF bleaching sequence with improved quality pulp.

Appreciable reduction in P.C. No./Yellowness was noticed. The detailed findings of the month long trial in Bagasse based fibre line are given in Table No. 2.

Samples of effluent discharge from the bleach plants as well as the final discharge from the mills were got analysed by the recognised outside laboratories. Appreciable reduction in terms of AOX was indicated. Company is in the process of procuring the necessary equipments for in-house testing of AOX.

The findings of blank vis-a-vis enzyme treated pulp w.r.t. AOX levels is given in Table No. 3. Though the Bleach plant effluents could not be separately investigated for B.O.D./C.O.D. loadings, no change was noticed in the final effluent discharge w.r.t. these parameters. Detailed studies for these will be undertaken during the next runs with enzyme.

ECONOMICS

The additional chemical cost of Enzyme Prebleaching in case of wood based pulping comes to around Rs. 200/- per ton and in case of Bagasse with "ECF" in the range of Rs. 345-415 per tonne which is expected to be at par incase of WPP and around Rs. 135-205 in case of Bagasse respectively if the new version of the product dosage @ 300 gms per tonne is established on the Plant scale.

The intangible gains in terms of improved products quality and appreciable reduction in AOX levels are not quantified.

CONCLUSION

Bio Bleaching followed by Peroxide bleaching stage offers an afforadable ECF bleaching system. Elimination of Elemental Chlorine from the Bleach plant without sacrificing on the pulp quality or any increase in the cost is feasible by incorporating Enzyme treatment.

In longer terms, this approach will gain paramount importance when pressure on limiting the Chlorinated organic compound in the effluents will rise. With optimisation of dosage and process conditions, Biobleaching could be a cost effective, viable technology for the Pulp and Paper Industry.

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